Lid-Driven Cavity Flow

In this work the Navier-Stokes equations, written in a ψ (stream-function)- ω (vorticity) formulation, are solved on a two dimensional Cartesian grid, in order to simulate the fluid flow in a square cavity with the upper wall moving at a constant velocity.

Equations

Indicating as V the velocity field (being *u* and *v* its components in *x* and *y* directions, respectively), we have:

$$\omega = rotV = \left(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x}\right) \kappa \quad (1) \text{ (Vorticity definition)}$$
$$u = \frac{\partial \psi}{\partial y} \qquad v = -\frac{\partial \psi}{\partial x} \quad (2) \text{ (Riemann equations)}$$

Combining eq. (1) and (2), we obtain:

$$\omega = \frac{\partial}{\partial x} \left(\frac{\partial \psi}{\partial x} \right) - \frac{\partial}{\partial y} \left(-\frac{\partial \psi}{\partial y} \right) = \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} = \nabla^2 \psi$$

$$\omega = \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} \qquad (3) \qquad (Poisson equation for the stream function)$$

We can now find the second necessary equation for solving the initial problem. To this aim, we start from the Navier Stokes equations:

$$\rho\left(\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j}\right) = -\frac{\partial P}{\partial x_i} + \mu \frac{\partial^2 u_i}{\partial x_j^2}$$

By taking the curl of the above equation (and after some algebra) we have:

$$\frac{\partial \omega}{\partial t} + u \frac{\partial \omega}{\partial x} + v \frac{\partial \omega}{\partial y} = \frac{1}{\text{Re}} \left(\frac{\partial^2 \omega}{\partial x^2} + \frac{\partial^2 \omega}{\partial y^2} \right)$$
(4) (vorticity-transport equation)

The equations we obtained, (1)-(4), can be numerically solved to compute the solution of the stated problem.

To this aim, we adopt a finite difference method on a Cartesian 2-Dimensional grid. In this way, the discretized form of eq. (1)-(4) is:

• Velocity components:

$$u_{i,j} \cong -\left(\frac{\psi_{i,j+1} - \psi_{i,j-1}}{2\Delta y}\right) \quad \text{and} \quad v_{i,j} \cong \left(\frac{\psi_{i+1,j} - \psi_{i-1,j}}{2\Delta x}\right)$$

• Vorticity transport

$$\omega_{i,j}^{n+1} = \omega_{i,j}^{n} + \Delta t \left[\left(-u_{i,j}^{n} \frac{\omega_{i+1,j}^{n} - \omega_{i-1,j}^{n}}{2\Delta x} - v_{i,j}^{n} \frac{\omega_{i,j+1}^{n} - \omega_{i,j-1}^{n}}{2\Delta y} \right) \right] + \frac{1}{\operatorname{Re}} \left(\frac{\omega_{i+1,j}^{n} - 2\omega_{i,j}^{n} + \omega_{i-1,j}^{n}}{\Delta x^{2}} + \frac{\omega_{i,j+1}^{n} - 2\omega_{i,j}^{n} + \omega_{i,j-1}^{n}}{\Delta y^{2}} \right)$$

• Poisson equation

$$\omega_{i,j}^{n} = \left(\frac{\psi_{i+1,j}^{n} - 2\psi_{i,j}^{n} + \psi_{i-1,j}^{n}}{\Delta x^{2}} + \frac{\psi_{i,j+1}^{n} - 2\psi_{i,j}^{n} + \psi_{i,j-1}^{n}}{\Delta y^{2}}\right)$$

(To solve this Poisson equation, one has to rewrite it in the form $\psi=f(\omega)$)

Boundary conditions

Equations (3) and (4) are elliptical partial differential equations. This make necessary to define boundary conditions in each side of the domain. We can use the following relations:

• Vertical side (Left) :

$$\omega_{1,j} = \frac{0.5}{dx^2} (8\psi_{2,j} - \psi_{3,j})$$

• Vertical side (Right) :

$$\omega_{nl+1,j} = \frac{0.5}{dx^2} (8\psi_{nl,j} - \psi_{nl-1,j})$$

• Horizontal side (bottom) :

$$\omega_{i,1} = \frac{0.5}{dy^2} (8\psi_{i,2} - \psi_{i,3})$$

• Horizontal side (top) :

$$\omega_{i,nh+1} = \frac{0.5}{dy^2} (8\psi_{i,nh} - \psi_{i,nh-1}) + \frac{3U}{dy}$$

(U is the velocity of the top wall)

Simulations and results

I report here a detailed list of the results I obtained for a simulation of the lid-driven cavity flow at Reynold number equal to 5000 on a 100x100 cartesian grid.

Simulations data	
Mesh	100x100
Reynolds number	5000
BC accuracy (for ω)	2° order
Simulation time step (dt)	10^-3
Tempo fittizio di simulazione	282.67seconds (282670 iterations)



Fig 1: Stream function (3-d surface) (max=3.5929e-003 ;min=-1.135e-001)

Stream Function



Fig 2: Stream function (isocontours)



Fig 3: Vorticity (isocontours)

Velocity field



Fig 4: Vector rapresentation of velocity field



Fig 5: u-component on the middle section



Fig 6:v-component on the middle section

Convergence



Fig 7:Plot of the "error" as a function of time

In Fig. 7 I plotted the value of the mean difference:

$$\boldsymbol{\omega}^{n+1} - \boldsymbol{\omega}^{n}$$

as a function of the simulation time.

It is necessary to mention that the simulation is stopped once the relation

$$\left|\omega_{\scriptscriptstyle i,j}^{\scriptscriptstyle n+1}-\omega_{\scriptscriptstyle i,j}^{\scriptscriptstyle n}\right|<10^{-6}$$

is verified.

In the following section I will present a detailed analysis of the stream function obtained for different simulations (by varying the Reynolds number). These results can be used as a benchmark to compare or validate some new algorithms.

<u>Streamfunction Analisys</u> (the tables below refers to the peaks of the stream function)

First Simulation: Reynolds Number=100 •



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
100	-0.1034	-	$1.7332 \cdot 10^{-6}$	$1.2490 \cdot 10^{-5}$	-

Second Simulation: Reynolds Number=500 •



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
500	-0.1147	_	$2.8668 \cdot 10^{-5}$	$8.8144 \cdot 10^{-4}$	-

• Third Simulation: Reynolds Number=1000



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
1000	-0.1173	-	$2.2917 \cdot 10^{-4}$	$1.8 \cdot 10^{-3}$	-

• Fourth Simulation: <u>Reynolds Number=2000</u>



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
2000	-0.1175	$1.0134 \cdot 10^{-4}$	$7.3392 \cdot 10^{-4}$	$2.6 \cdot 10^{-3}$	-

• Fifth Simulation: Reynolds Number=5000



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
5000	-0.1135	$1.3 \cdot 10^{-3}$	$1.3 \cdot 10^{-3}$	$3.6 \cdot 10^{-3}$	$-3.7995 \cdot 10^{-6}$

• Sixth Simulation: Reynolds Number=7500



Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
7500	-0.1099	$1.9 \cdot 10^{-3}$	$1.5 \cdot 10^{-3}$	$4.2 \cdot 10^{-3}$	$-8.8889 \cdot 10^{-5}$

Reynold	Primary	Upper left	Lower left	Lower right	Secondary lower right
S	vortex	vortex	vortex	vortex	vortex
100	-0.1034	-	$1.7332 \cdot 10^{-6}$	$1.2490 \cdot 10^{-5}$	-
500	-0.1147	-	$2.8668 \cdot 10^{-5}$	$8.8144 \cdot 10^{-4}$	-
1000	-0.1173	-	$2.2917 \cdot 10^{-4}$	$1.8 \cdot 10^{-3}$	-
2000	-0.1175	$1.0134 \cdot 10^{-4}$	$7.3392 \cdot 10^{-4}$	$2.6 \cdot 10^{-3}$	-
5000	-0.1135	$1.3 \cdot 10^{-3}$	$1.3 \cdot 10^{-3}$	$3.6 \cdot 10^{-3}$	$-3.7995 \cdot 10^{-6}$
7500	-0.1099	$1.9 \cdot 10^{-3}$	$1.5 \cdot 10^{-3}$	$4.2 \cdot 10^{-3}$	$-8.8889 \cdot 10^{-5}$

Summary of the results (stream function peaks)