



Tube Bundle

A simple shell model for the break-up of agglomerates in turbulent flows

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Dynamics of non-spherical particles



Outline

- Escape of particles from potential wells
 - Role of the turbulence
 - Removal rate
 - Rock n roll model
- Characterising agglomerates
- Shell model for breakup
- Prediction versus experimental results

 ARTIST experiment





- *p*, the resuspension rate constant *ω*, the typical frequency of vibration, *Q* height of adhesive potential well,
- *<PE>* average potential energy of particle in the well.



Particle escape from potential well

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Fraction remaining after 1 sec

and resuspension rate: $f_R(t) = \int_0^\infty e^{-p(f'_a)t} \varphi(f'_a) df'_a$ $\Lambda(t) = \int_0^\infty p(f_a') e^{-p(f_a')t} \varphi(f_a') df_a'$ $p = \frac{\omega_0}{2\pi} \exp\left(-\frac{k(f_a - \langle F \rangle)^2}{\langle f^2 \rangle (1+\eta)}\right)$ f_a = adhesive force F_a = adhesive for perfect contact $F_a = 3\pi\gamma r$, $\gamma = \text{surface energy}$, r = particle radius $f'_a = f_a / F_a$; $\varphi(f'_a)$ Lognormal distribution Biasi *et al.* (2001) $\langle f'_a \rangle = 0.016 - 0.0023r^{0.545}$ $\sigma'_{a} = 1.8 + 0.136r^{1.4}$, r in microns



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Short and long term removal rates



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Mehanism for Agglomerate breakup

• Rupture

- Break-up into fragments -daughter agglomerates
- simialr to particle removal from a surface
 - Threshold for aerodynamic forces based on strength of agglomerate
 - Continues until agglomerates reaches a minimum size
 - Usually 3 or 4 daughter fragments

• Erosion

- Lower aerodynamic forces than rupure
- Much slower than breakup due to rupture
- Onion peeling mechanism
- Use of kinetic / stochastic models



Characterising an Agglomerate

For a fractal agglomerate, the number of primary particles within the agglomerate is given by:

$$N_{P} = k_{o} \left(R_{c} / r_{p} \right)^{d_{f}}$$

 $k_o \approx 0.42 d_f - 0.22$ in the range $1.50 \le d_f \le 2.75$

 d_f is the fractal dimension. R_c is the collision or outer radius r_p is the primary particle radius

volume fraction of the particle

$$\phi = \frac{V_m}{V_P}$$

 V_m is the material volume V_p is the volume of the particle the material and void volume



$$\phi(r) = k_o \frac{d_f}{3} \left(\frac{r}{r_p}\right)^{d_f - 3}$$

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Characterising agglomerate

The average thickness of the *l*-th shell Δr_l will depend upon the volume fraction and the

distribution of particles sizes within each shell. It is given by

The *l*-th shell outer radius is then defined as:

$$\mathbf{R}_{l} = \mathbf{r}_{p} + \sum_{i=1}^{l} \overline{\Delta \mathbf{r}_{i}}$$

And the radius of the l-th shell which is half way between the outer and inner radii of the shell is then:

$$r_l = \frac{1}{2} \left(R_l + R_{l+1} \right)$$

The number of particles in the *k*-th shell is given by:

$$\overline{n_{pl}} = N_p(r_{l+1}) - N_p(r_l)$$

 $\overline{\Delta r_l} = \left(\frac{v_p}{\phi(R_{l+1})}\right)^{\frac{1}{3}}$



Equations for the breakup rate

 $p(\xi)$ is the rate constant for removal of particles from an adhesive potential well characterised by ξ

The total removal rate of particles being an integration over a broad range of adhesive potential, i.e. values of ξ due to a distribution of particle sizes, microscale roughness and flow exposure

The removal rate of particles from any given shell/layer depends upon the rate at which particles are are exposed to the flow by removal of particles from the shell above

If $n_i(\xi, t) d\xi$ is the number of particles in the layer *i* with adhesive and flow parameters between ξ , $\xi + d\xi$, with pdf $\psi(\xi)$

$$\begin{aligned} \frac{\partial n_i(\xi,t)}{\partial t} &= -p(\xi)n_i(\xi,t) + \psi(\xi) \int_0^\infty p(\xi')n_{i-1}(\xi',t)d\xi' \\ &= -p(\xi)n_i(\xi,t) + \psi(\xi)\Lambda_{i-1}(t) \end{aligned}$$



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rms fluctuating drag force

RMS flow velocities in the radial (longitudinal) and azimuthal (lateral) directions for

$$\sqrt{\overline{v_r^2}} = \sqrt{\overline{v_\theta^2}} = \left(\overline{\dot{\gamma}^2}\right)^{1/2} r / \sqrt{2}$$

rms radial drag force

$$e \quad \sigma^2 = \frac{1}{2} \dot{\gamma}^2 \beta_\tau^2 r^2,$$

The adhesive force f_a is selected from a lognormal distribution

$$\varphi(f_a) = \frac{1}{\sqrt{2\pi}} \left(\frac{1}{f_a \ln \sigma_a} \right) \exp \left(-\frac{1}{2} \left[\frac{\ln(f_a)}{\ln \sigma_a} \right]^2 \right)$$



 f_a is normalized by the Van der Waals force F_a between 2 spheres in perfectly smooth contact, which is, according to Equation (2.53), $F_a = \frac{3}{2}\pi\Gamma_a r_a$ and reduced by a factor of the order 100 due to the roughness of the contact

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Distribution of clusters within agglomerate

Figure 8.3: Fragment Size distribution obtained experimentally compared to the reconstructed fragmer size distribution based on the coordination distribution



Agglomerates are fragments 48% triplets, 22% quartets, 25% quintets, ...

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Shell removal removal rates







experimental results and model predictions



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Summary & conclusions

- Model for agglomerate break up
 - Analogous to removal of a particles from surfaces in turbulent boundary layers
 - Escape of particles from adhesive potential wells
 - Motion driven by fluctuating aerodynamic forces/ moments
 - Rock and roll about surface asperities
 - Shell model similar to multilayer resuspension
 - removal particles from any shell/leer rate limited by removal of particles from the layer above
 - Future developments
 - DNS of flows within agglomerates
 - Calculation of forces on individual primary particles