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Numerical modeling of air–fiber flows

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Industrial application

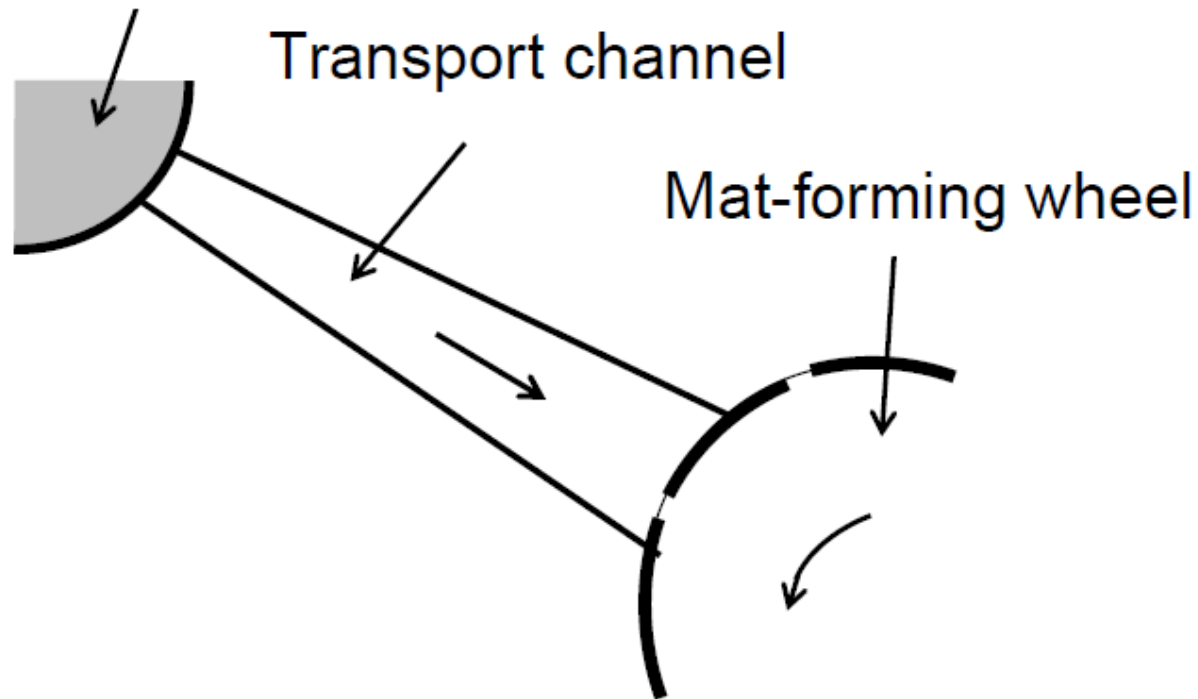
Absorbent hygiene products (diapers, sanitary napkins)



Core of product: Fibers

Fibers transported by flowing air and deposit on forming wheel

Milling machine



Uniform spatial fiber distribution on mat ensures product quality

Present work

Fundamental studies of fiber-flow dynamics

- Rheology of sheared fiber suspensions
- Fiber flocculation in turbulent flow field

Numerical method

Microhydrodynamics approach: Particle-level simulation technique

- Accounting for realistic fiber features: deformability, different shapes
- Inclusion of various forces: fiber-flow, fiber-fiber interactions
- Detailed information about fiber suspension: positions, orientations

Particle-level fiber model

- Chain of rigid cylindrical segments
- Each segment tracked individually – LPT
- Segment inertia taken into account
- Flexible and rigid fibers

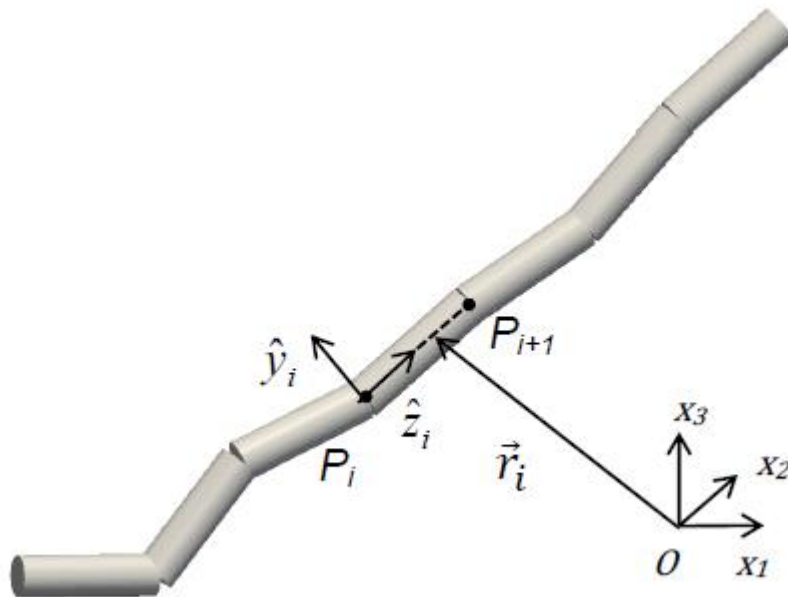
Schmid *et al.* (*J. Rheol.*, 2000)

Lindström and Uesaka (*Phys. of Fluids*, 2007)

Fiber geometry

Chain of rigid cylindrical segments

Geometrical properties defined for **each segment**



- diameter
- length
- position vector
- unit direction vectors
- equilibrium shape

Flexible fiber equations of motion

Direct application of Euler's laws for **each fiber segment**

- Linear momentum equation

h : hydrodynamic

$\mathbf{X}$: connectivity force

$$m_i \ddot{\mathbf{r}}_i = \mathbf{F}_i^h + \mathbf{X}_{i+1} - \mathbf{X}_i$$

- Angular momentum equation

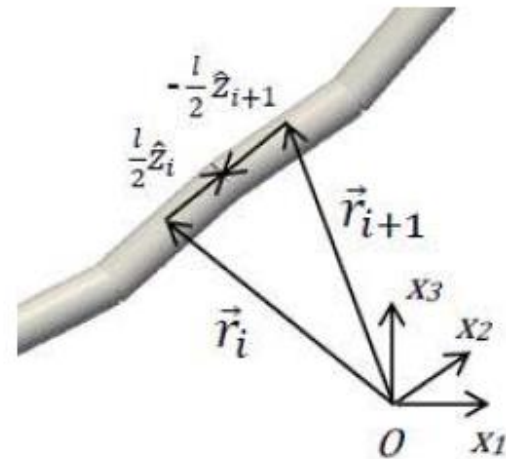
$$\frac{\partial(\mathbf{I}_i \cdot \boldsymbol{\omega}_i)}{\partial t} = \mathbf{T}_i^h + \mathbf{Y}_{i+1} - \mathbf{Y}_i + \frac{l_i}{2} \hat{\mathbf{z}}_i \times \mathbf{X}_{i+1} + \left(\frac{-l_i}{2} \hat{\mathbf{z}}_i \right) \times (-\mathbf{X}_i)$$

$\mathbf{Y}$: sum of bending and twisting torques

Flexible fiber equations of motion (cont.)

- Connectivity constraint - end points of adjacent segments coincide

$$\mathbf{r}_i + \frac{l_i}{2} \hat{\mathbf{z}}_i = \mathbf{r}_{i+1} - \frac{l_{i+1}}{2} \hat{\mathbf{z}}_{i+1}$$



- Connectivity equation - time derivative of connectivity constraint

$$\dot{\mathbf{r}}_{i+1} - \dot{\mathbf{r}}_i = \frac{l_i}{2} \boldsymbol{\omega}_i \times \hat{\mathbf{z}}_i + \frac{l_{i+1}}{2} \boldsymbol{\omega}_{i+1} \times \hat{\mathbf{z}}_{i+1}$$

Connectivity force linear system

- Time discretization (implicit numerical scheme)
- Dimensionless equations to ensure numerical stability

$$\begin{bmatrix} S_{1,n-1}^* & T_{1,n-1}^* & 0 & 0 & 0 & 0 \\ Q_{2,n-1}^* & S_{2,n-1}^* & T_{2,n-1}^* & 0 & 0 & 0 \\ 0 & Q_{3,n-1}^* & S_{3,n-1}^* & T_{3,n-1}^* & 0 & 0 \\ 0 & 0 & Q_{4,n-1}^* & S_{4,n-1}^* & T_{4,n-1}^* & 0 \\ 0 & 0 & 0 & Q_{5,n-1}^* & S_{5,n-1}^* & T_{5,n-1}^* \\ 0 & 0 & 0 & 0 & Q_{6,n-1}^* & S_{6,n-1}^* \end{bmatrix} \cdot \begin{bmatrix} X_{2,n}^* \\ X_{3,n}^* \\ X_{4,n}^* \\ X_{5,n}^* \\ X_{6,n}^* \\ X_{7,n}^* \end{bmatrix} = \begin{bmatrix} V_{2,n-1}^* \\ V_{3,n-1}^* \\ V_{4,n-1}^* \\ V_{5,n-1}^* \\ V_{6,n-1}^* \\ V_{7,n-1}^* \end{bmatrix}$$

Linear system for connectivity forces for 7-segment fiber

- Solve velocities and angular velocities
- Evolve segment positions and orientations in time

Rigid fiber equations of motion

Formulated for fiber's center of mass (contributions summed over segments)

- Linear momentum equation

$$m\ddot{\vec{r}}_G = \sum_i \vec{F}_i^h$$

- Angular momentum equation

$$\bar{\vec{I}}_G \cdot \dot{\vec{\omega}} + \vec{\omega} \times (\bar{\vec{I}}_G \cdot \vec{\omega}) = \sum_i \{ \vec{T}_i^h + \vec{r}_{Gi} \times \vec{F}_i^h \}$$

- Solve translational velocities and angular velocity
- Evolve segment positions and orientations in time

Rheology of sheared fiber suspensions

Understanding suspension structure

- Process optimization, product quality

Rigid, straight fibers

- Batchelor's theory – known fiber orientation
- Semi-dilute suspensions; hydrodynamic interactions

Flexible fibers, fibers with irregular equilibrium shapes

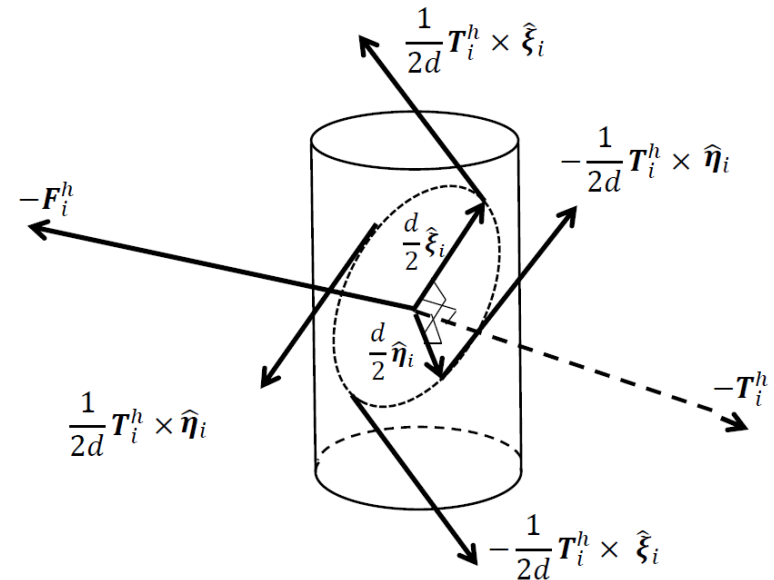
- No theoretical studies
- Few numerical studies – based on Batchelor's theory

Rheology of sheared fiber suspensions:

Direct method for deviatoric stress computation

- Dipole strength of single fiber
- Hydrodynamic forces and torques as localized tractions

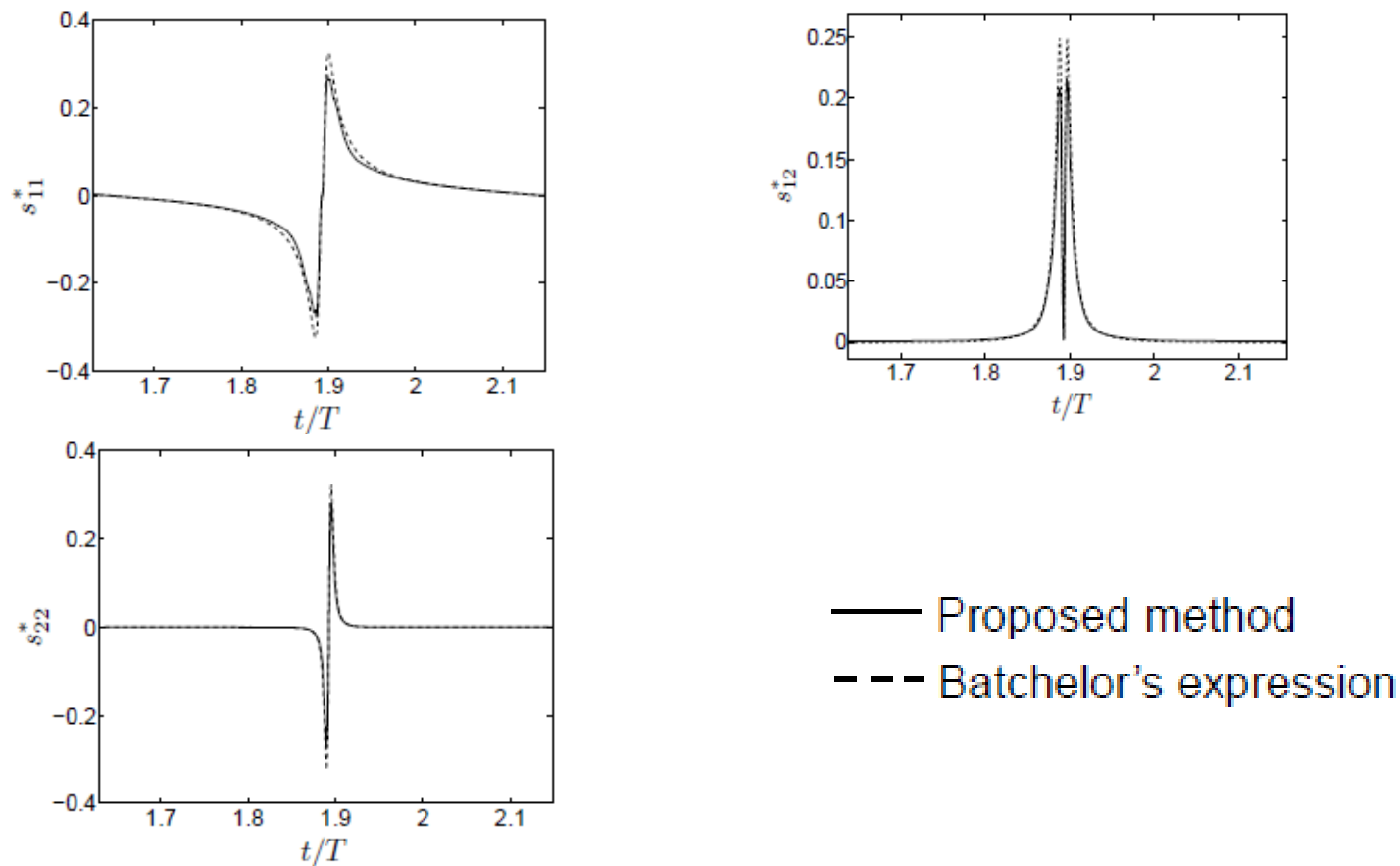
$$\begin{aligned}
 s' &= \iint_A [\boldsymbol{\tau} \mathbf{r} - \frac{1}{3}(\mathbf{r} \cdot \boldsymbol{\tau}) \boldsymbol{\delta}] dA \\
 &= \sum_{i=1}^N [F_i^h \mathbf{r}_i + \frac{1}{2} \boldsymbol{\epsilon} \cdot \mathbf{T}_i^h - \frac{1}{3}(\mathbf{r}_i \cdot \mathbf{F}_i^h) \boldsymbol{\delta}]
 \end{aligned}$$



- Flexible fibers
- Fibers with irregular equilibrium shapes

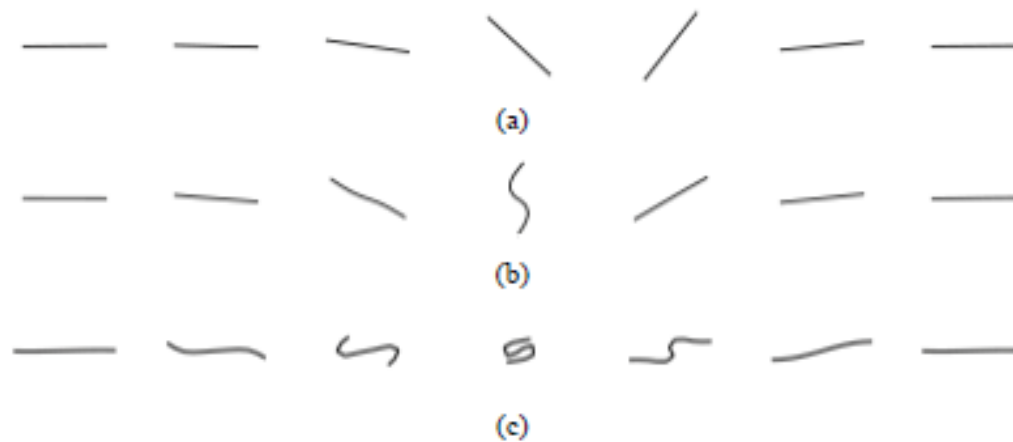
Rheology of sheared fiber suspensions: Dipole strength validation

Isolated, straight, rigid fiber – agreement with Batchelor's theory



Rheology of sheared fiber suspensions: Numerical experiments

- Ergodicity assumption; Fibers initially in flow-gradient plane
- Initially straight fibers – S-shape deformations

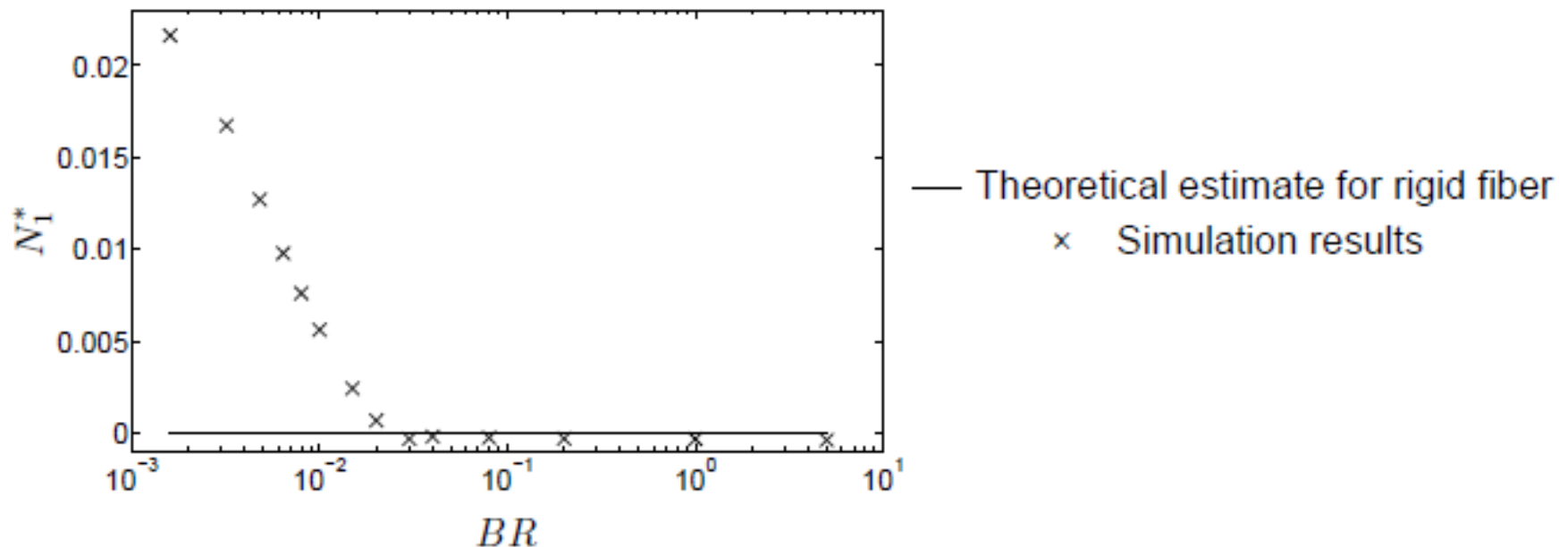


Time-series of images from simulation for different bending ratio:

a) $BR=1$, b) $BR=0.02$, c) $BR=0.0016$.

Rheology of sheared fiber suspensions: Effects of fiber flexibility

Relation between fiber bending ratio BR and first normal stress difference N_1^*

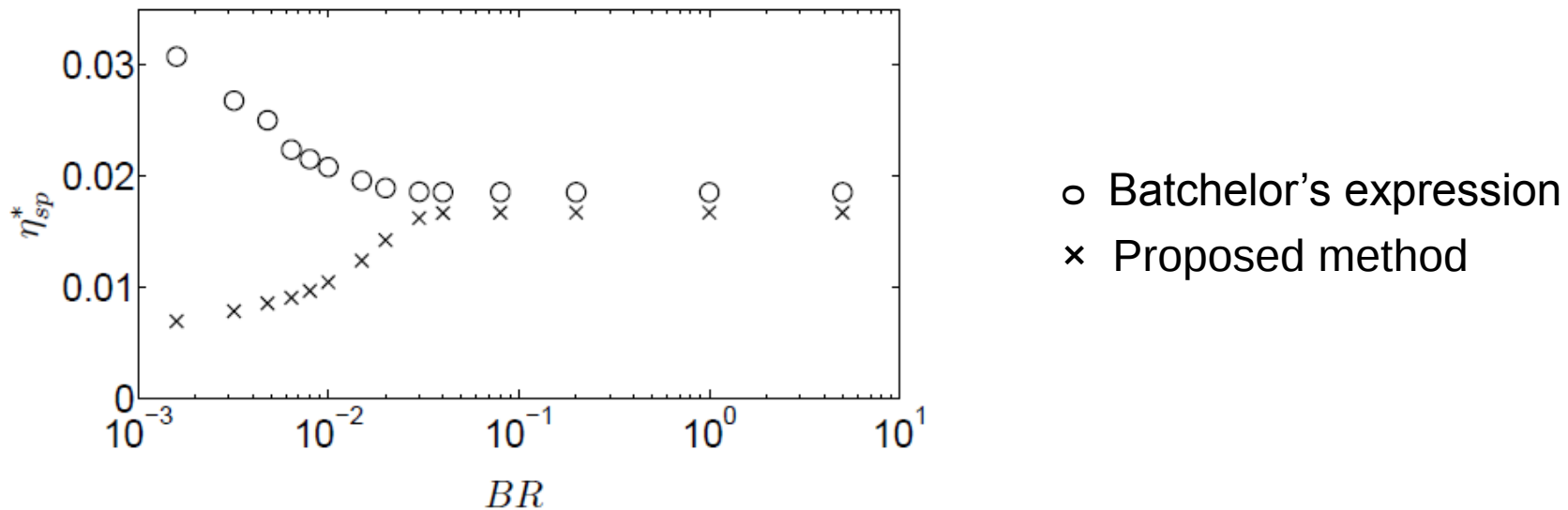


- Increases with fiber flexibility (lower BR values)

Rheology of sheared fiber suspensions:

Effects of fiber flexibility

Relation between fiber bending ratio BR and specific viscosity (SV) η_{sp}^*



- Batchelor's theory: SV increases with fiber flexibility
 - Observed by other studies (Joung *et al.*, *J. Non-Newtonian Fluid Mech.*, 2001)
- Proposed method: SV decreases with fiber flexibility
 - Reason: reduced viscous dissipation

Fiber flocculation in realistic flow fields

Geometries and flow conditions representative for industrial process

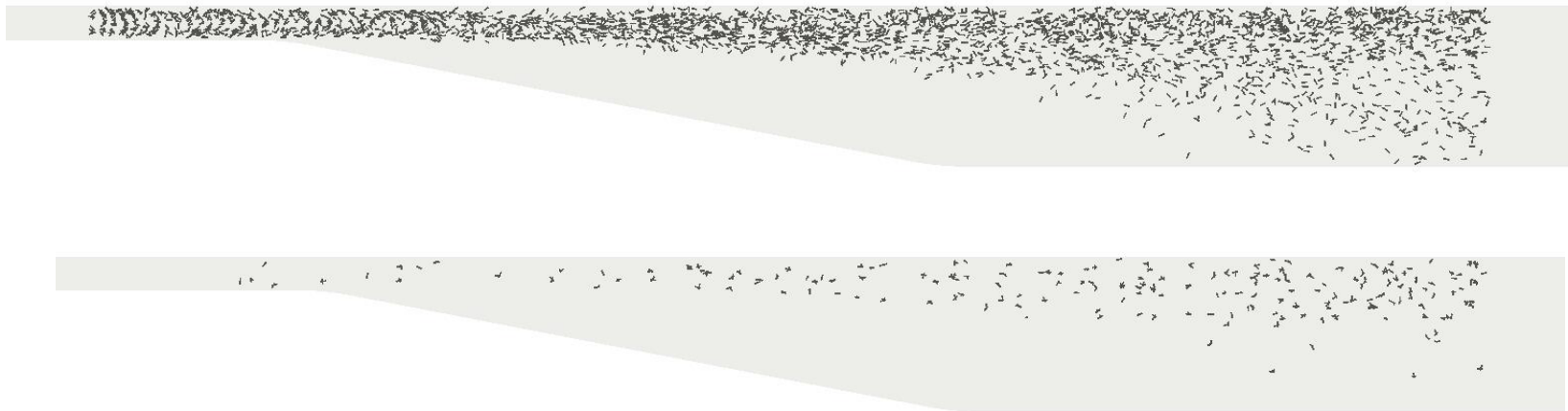
- Asymmetric planar diffuser
- High Reynolds number flow
- Non-creeping fiber-flow interactions

Fiber properties consistent with those of hardwood fibers

- Diameter, length, density

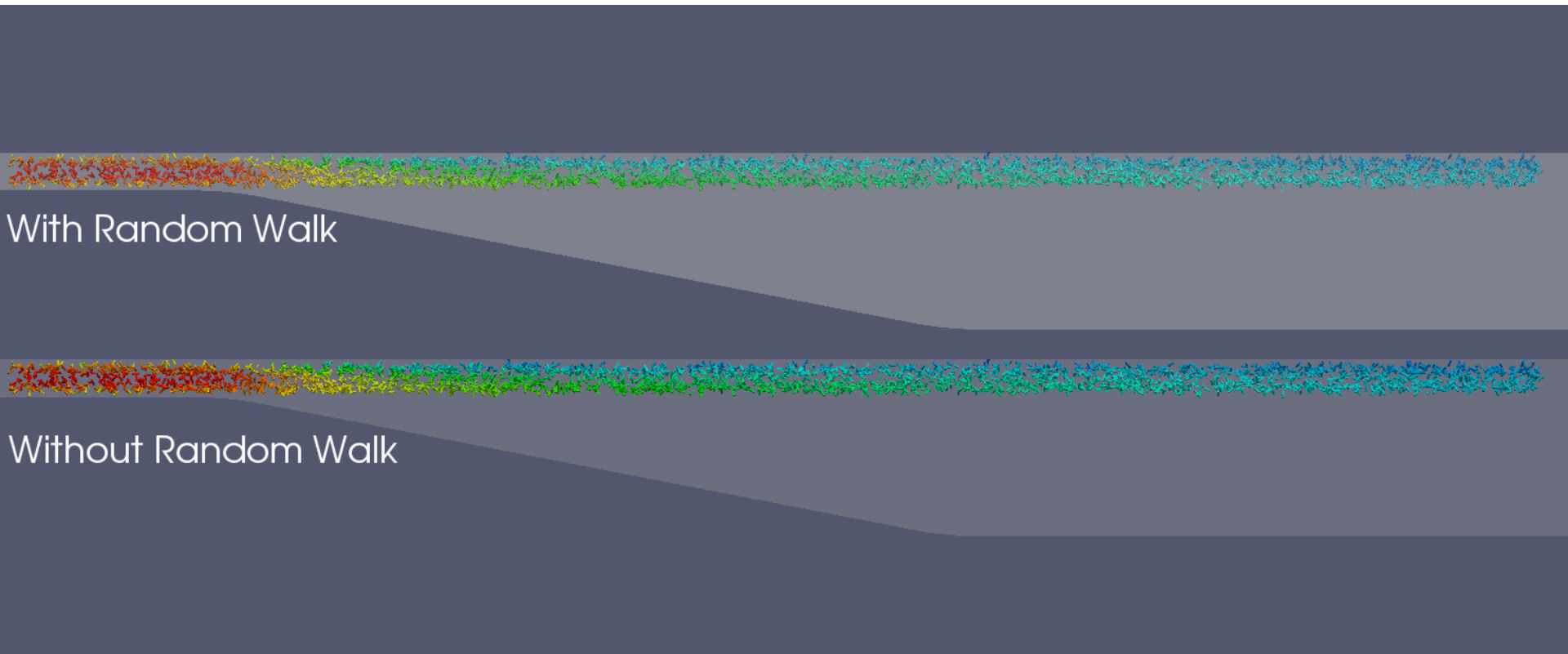
Fiber flocculation in realistic flow fields

- Dilute suspension of rigid, straight fibers
- Turbulent dispersion – stochastic model
- Short-range attractive forces – fibers interlock in flocs



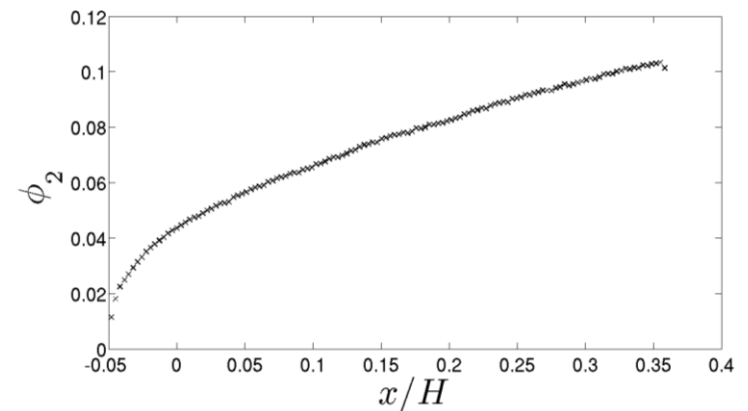
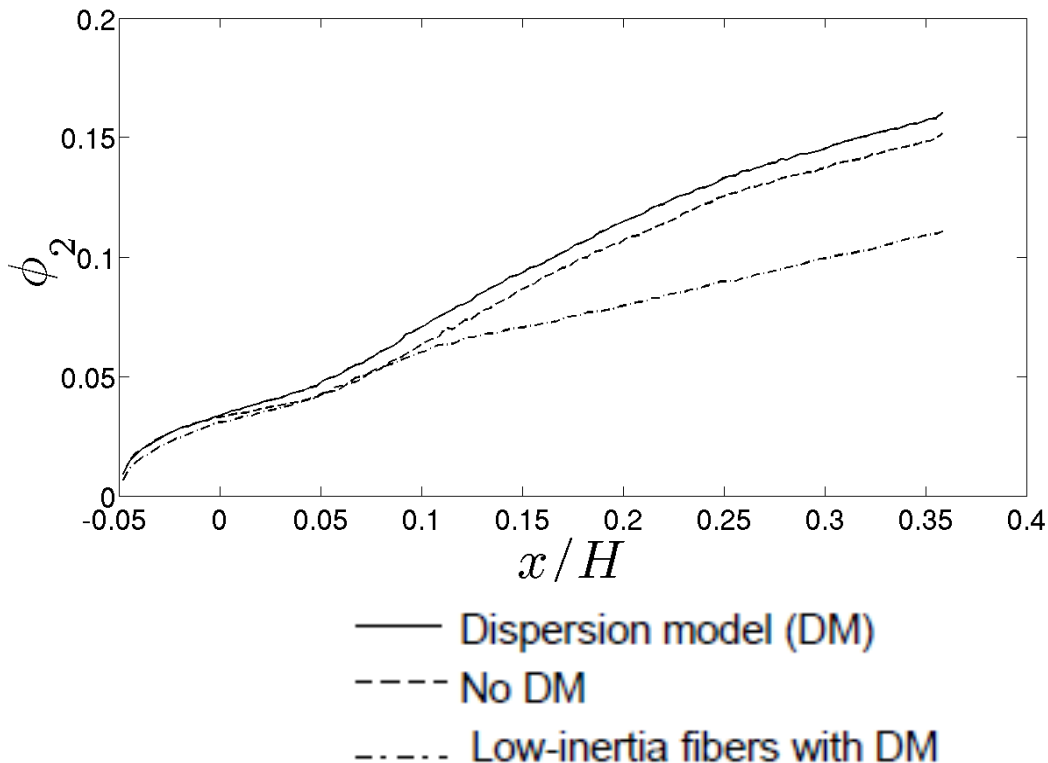
Fibers and fiber flocs – steady state solution

Top: all fibers; **Bottom:** fibers in flocs



Fiber flocculation in realistic flow fields

Variation of flock mass fraction ϕ_2 along diffuser



Straight channel with DM

Darting fiber motion → enhances collisions → increase in flocculation rate

Conclusions

- Rheology of flexible fiber suspensions
 - Viscosity decreases with fiber flexibility
 - Important to properly account for fiber deformability
 - Experimentalist – characterize fiber morphology
- Flocculation of rigid, straight fibers in turbulent flow
 - Darting fiber motion enhances collisions and flocculation rate

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Thank you!

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