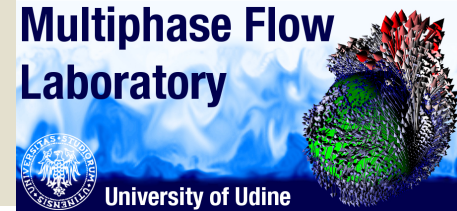


COMETE Training School on Direct numerical simulation
of solid particles, droplets and bubbles in turbulence

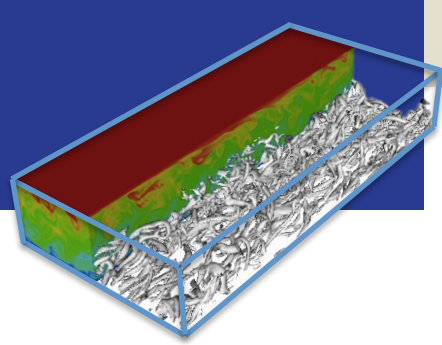


Collective particle dynamics in turbulent flows

Cristian Marchioli
University of Udine & CISM

Wien 11-13 February 2020



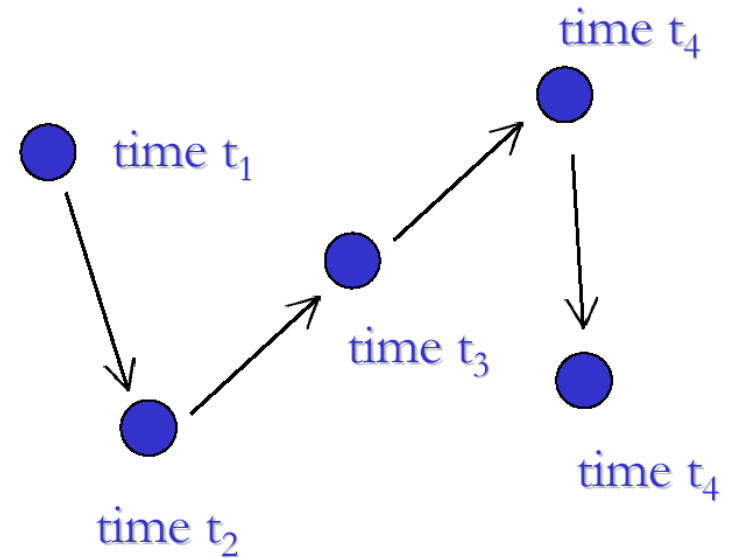
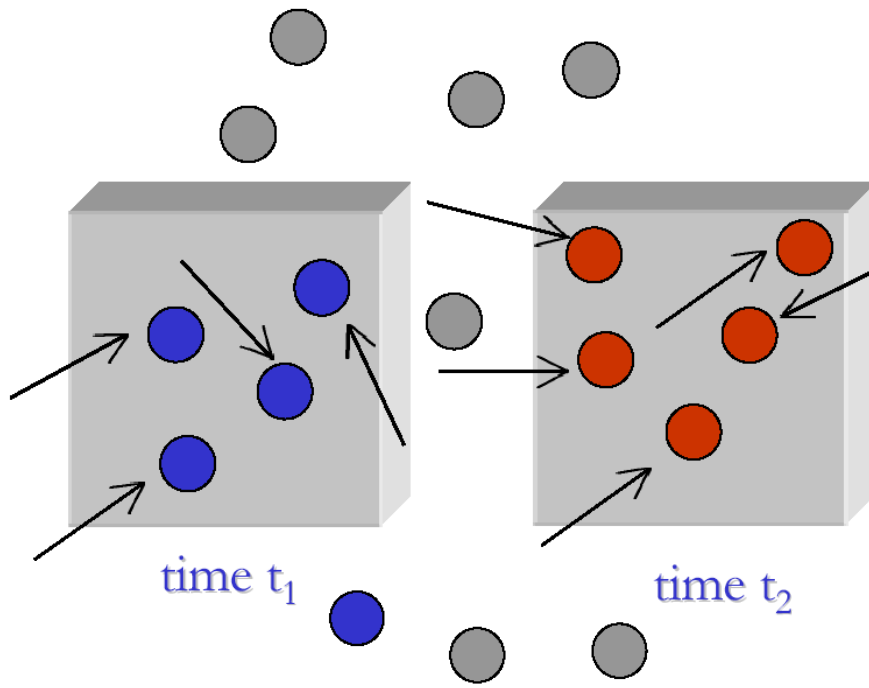


Euler-Lagrange description of particle-laden turbulent flows

Eulerian vs Lagrangian Modelling

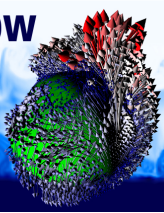
Eulerian Approach:

Focus on control volume

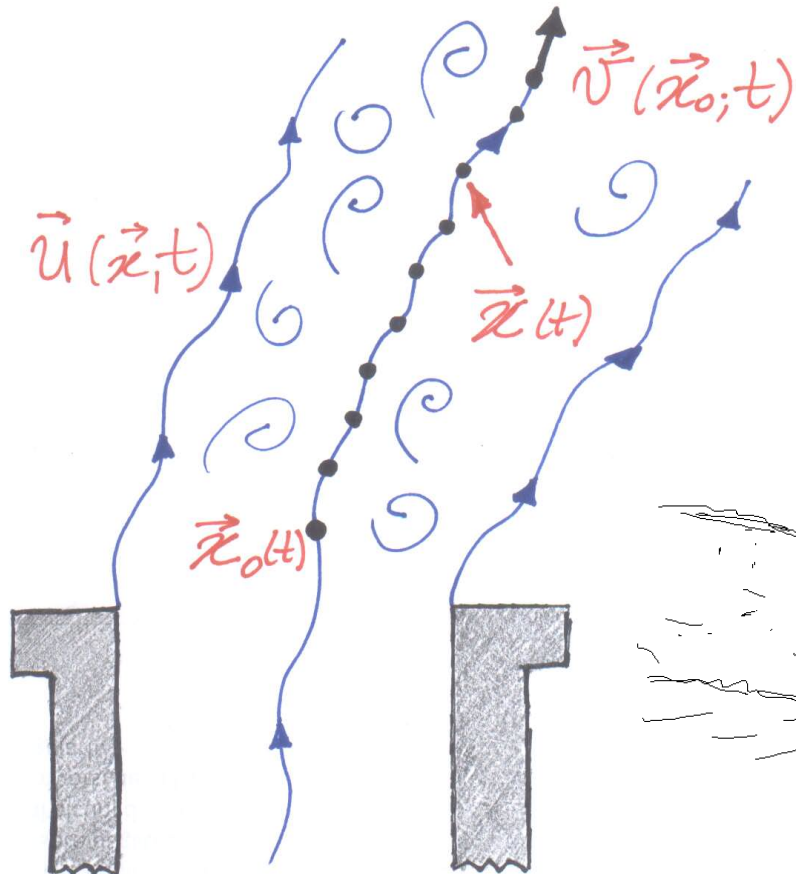
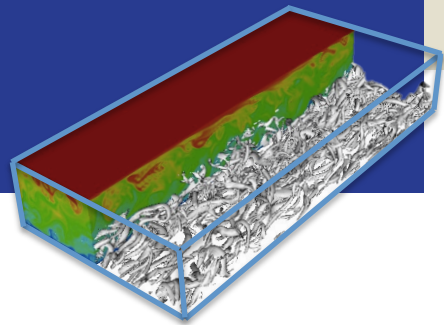


Lagrangian Approach:

Focus on particle trajectory

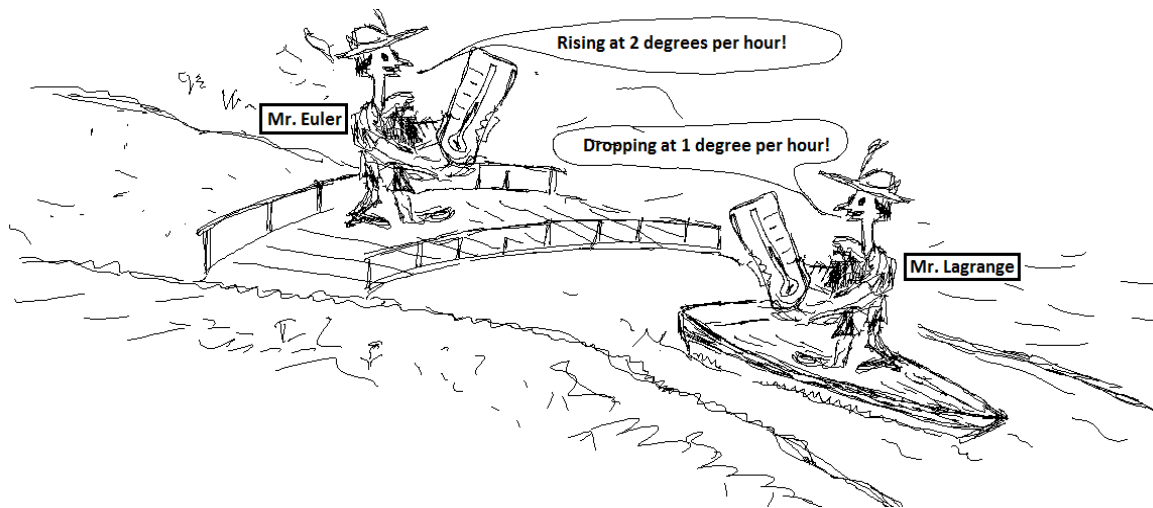


Eulerian vs Lagrangian Modelling



Eulerian approach: Focus is on the velocity at fixed control volumes points in the flow where one sees different particles at a time.

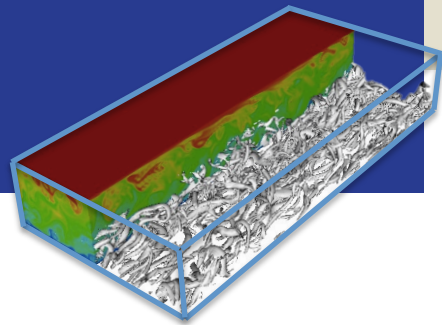
Lagrangian approach: Focus is on individual fluid particles, followed along their trajectory.



www.flowillustrator.com



Main approaches to the numerical simulation of turbulence



Reynolds Averaged Techniques

- Need extensive empirical data for constants
- Geometry specific
- Underlying assumption of isotropy (sometimes)

Volume Averaging (LES)

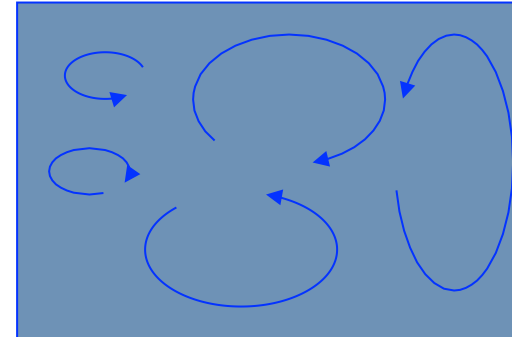
- Resolve the large eddies
- Average over small scales
- Simple universal models (maybe)

Direct Numerical Simulation (DNS)

- Valid for resolution finer than smaller eddies
- Applicable to low Reynolds number turbulent flows (computational cost limitations)

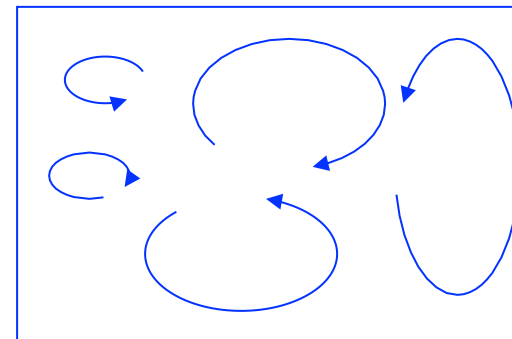
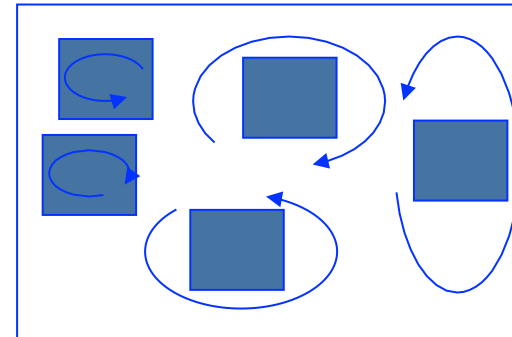
$$\langle u_i^l u_j^l \rangle$$

$$\langle u_i^l T^l \rangle$$



$$\overline{u_i^l u_j^l}$$

$$\overline{u_i^l T^l}$$



Accuracy / Computational cost

“Amount” of modeling

Eddy size and frequencies: A “dimensional” example

Water flowing through a pipe with 50 mm diameter at velocity 1.8 m/s.

$$Re \approx 10^5$$

“Type” of Eddy:	Size	Frequency
Largest Eddies	25 mm	3.5 Hz
Energy Containing Eddies	0.6 mm	140 Hz
Most Dissipative Eddies	0.125 mm = 125 μm	450 Hz
Kolmogorov Eddies	0.025 mm = 25 μm	1300 Hz

Computational cost for a DNS:

$$\left(\frac{L}{\eta_K}\right)^3 \left(\frac{T}{\tau_K}\right) \propto Re^{3.6} \left\{ \begin{array}{l} N_x \times N_y \times N_z \propto Re^{2.7} \\ N_t \propto Re^{0.9} \end{array} \right.$$

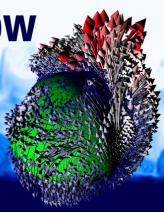
Compare computational costs: DNS vs LES

Grid resolution requirements for LES of turbulent boundary layers
(see Piomelli, *Philos Trans A Math Phys Eng Sci*, vol. 372, 2014):

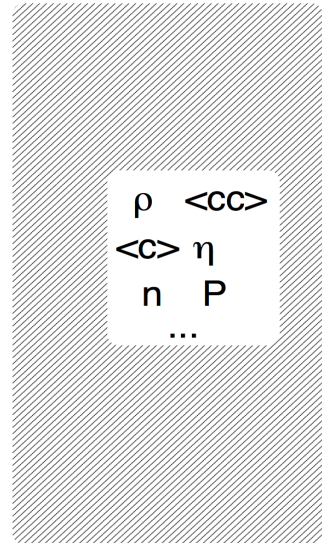
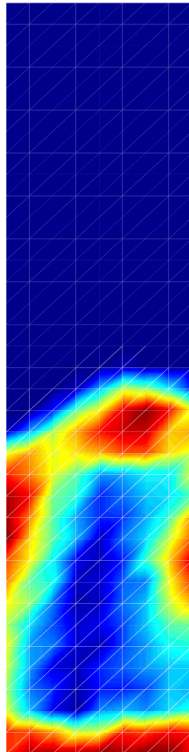
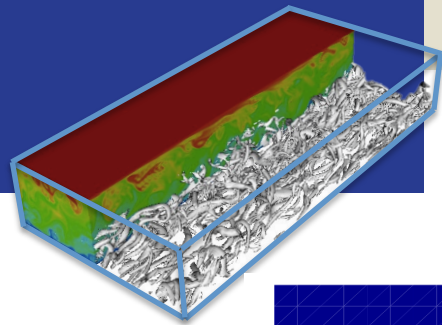
“Type” of LES	Spatial resolution
Resolve outer layer eddies (domain $L_x \times L_y \times d$)	$\propto Re^{0.4}$
Resolve inner layer eddies (wall-resolved LES)	$\propto Re^{1.8}$
LES with wall models	$\propto Re$

with δ = boundary layer thickness (separates inner and outer layer)

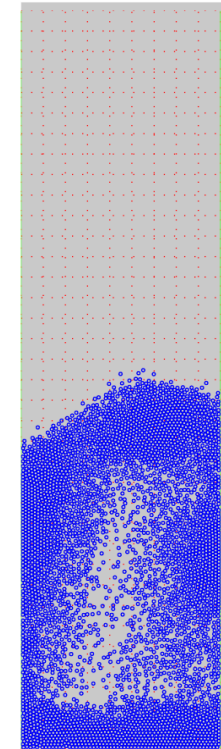
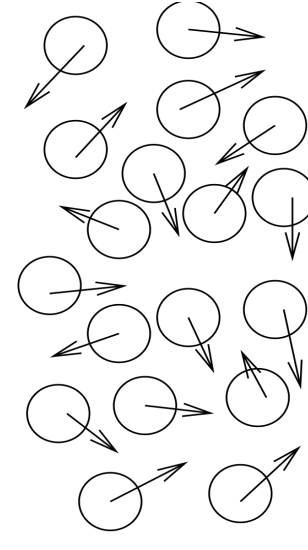
Total computational cost for a LES: up to $Re^{2.4}$



Lagrangian description of particles

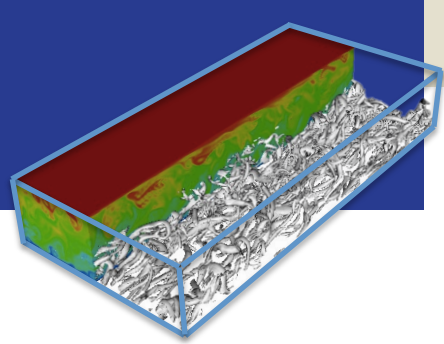


←
Coarse
graining



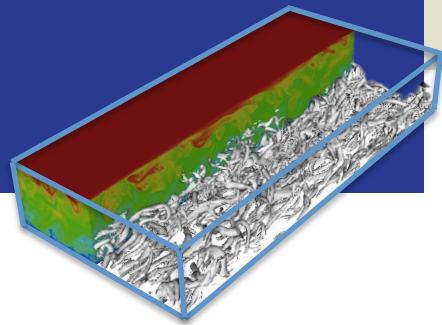
Eulerian Approach: use separate Eulerian balance equations for both phases (treated as two inter-penetrating continua), coupled through inter-phase exchange terms.

Lagrangian Approach: the trajectory of each particle and subsequent averaging (over all tracked particles) is simulated explicitly.



Lagrange tracking of pointwise particles

Forces Acting on a Particle



Drag

Gravity & Buoyancy

$$\frac{d m_p \mathbf{v}_p}{d t} = - 3 \pi d_p \mu (\mathbf{v}_p - \mathbf{v}) + (m_p - m_f) \mathbf{g}$$

Particle
Inertia

$$+ m_f \frac{D\mathbf{v}}{D t} - \frac{1}{2} m_f \left(\frac{d\mathbf{v}_p}{d t} - \frac{D\mathbf{v}}{D t} \right)$$

Added
Mass

$$- \frac{3}{2} \pi d_p^2 \mu \int_0^t \left(\frac{d\mathbf{v}_p}{d\tau} - \frac{d\mathbf{v}}{d\tau} \right) \frac{d\tau}{[\pi \nu (t-\tau)]^{0.5}}$$

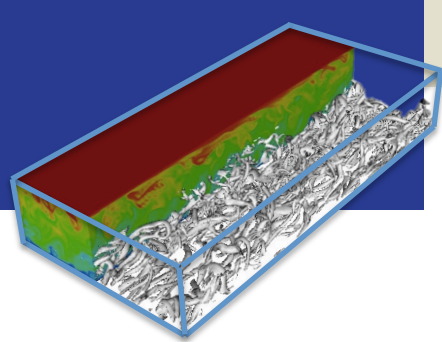
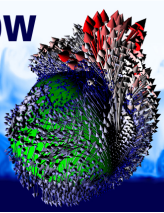
$$[+ m_f C_L (\mathbf{v} - \mathbf{v}_p) \times \boldsymbol{\omega}]$$

Pressure
Gradient

Lift

Basset
(history)

See: Poisson (1831); Stokes (1845); Basset (1888); Oseen (1911); Faxen (1922); Gatignol (1983); Maxey & Riley (1983)



Forces Acting on a Particle

$$F_{drag} \rightarrow O(St^{-1})$$

$$F_{prgr} \rightarrow O\left(\frac{\rho_f}{\rho_p}\right)$$

$$F_{addm} \rightarrow O\left(\frac{\rho_f}{\rho_p}\right)$$

Good news:

for small heavy particles only drag and gravity matter!!

Effect of other forces on particle motion is negligible.

$$F_{Bass} \rightarrow O\left(\left(\frac{\rho_f}{\rho_p}\right)^{1/2}\right)$$

$$F_{lift} \rightarrow O\left(d_p^2 \frac{\sqrt{dv/dy}}{v}\right)$$

Minimal “Stokesian” model for Lagrangian Particle Tracking

In the limit of small (pointwise) heavy particles:

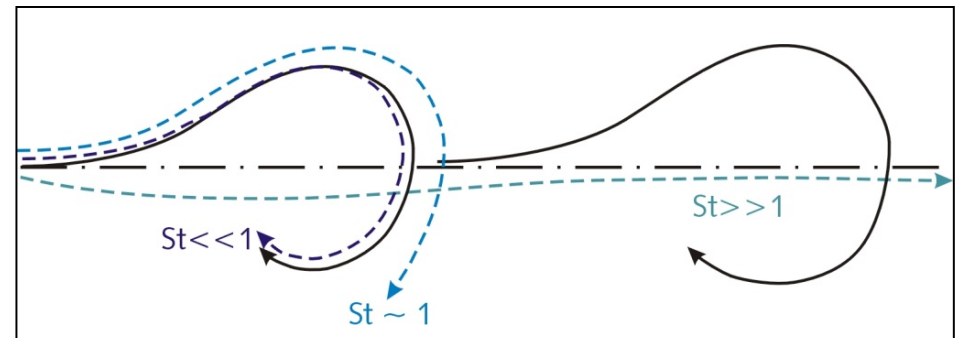
$$\frac{d\mathbf{v}_p}{dt} = \frac{\mathbf{v} - \mathbf{v}_p}{\tau_p \cdot f(\text{Re}_p)} - \mathbf{g} \left(1 - \frac{\rho_f}{\rho_p} \right)$$

Controlling parameters: τ_p and Re_p

Particle Timescale: $\tau_p = d_p^2 \rho_p / 18 \mu$

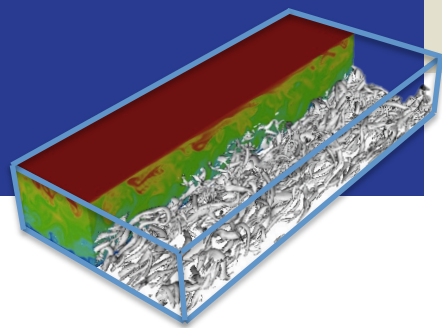
Flow Timescale: $\tau_f = L/U = \nu / u_\tau^2$

Particle Stokes number: $\text{St} = \tau_p / \tau_f$



Recall: in such minimal model, inertia controls
particle dynamics and particle-turbulence interactions

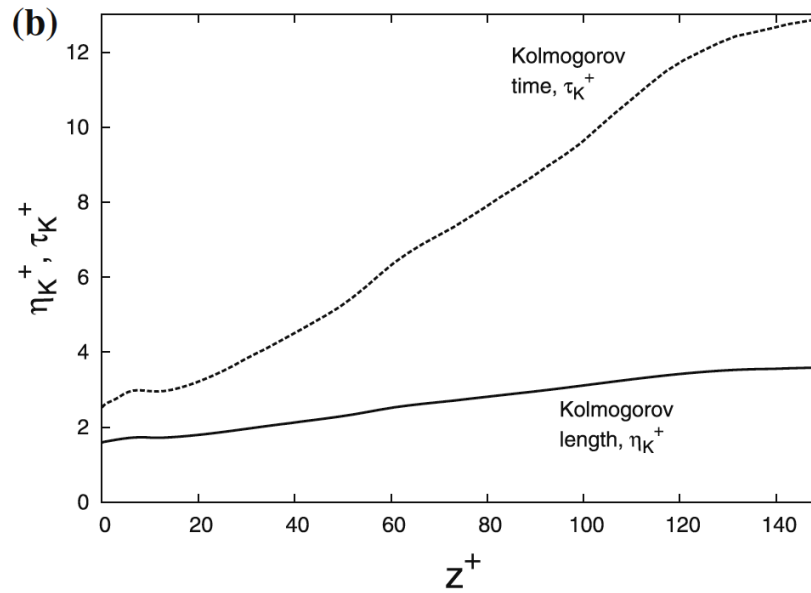
Flow anisotropy effects on fluid flow time scales



Kolmogorov time/length:

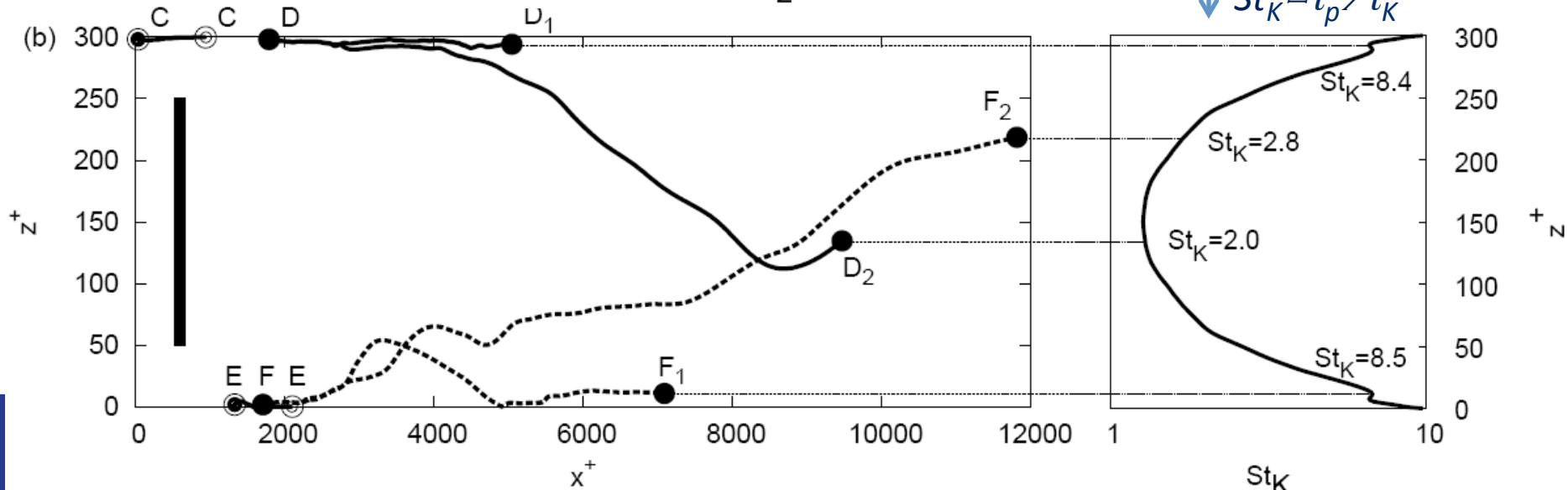
$$\tau_K^+ = \tau_K / \tau_f$$

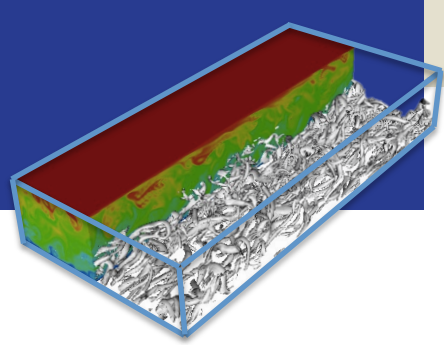
$$\eta_K^+ = \eta_K / \eta_f$$



Renormalized Stokes number:

$$St_K = \tau_p / \tau_K$$

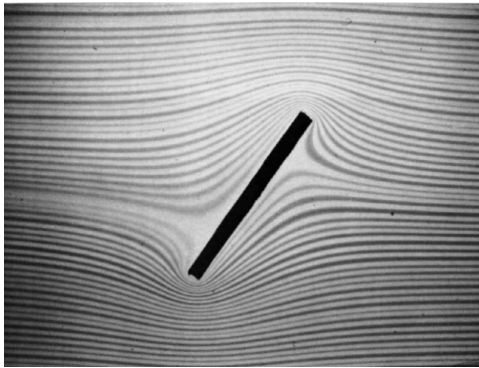




Lagrange tracking of non-spherical pointwise particles

Modelling non-spherical particles as pointwise particles

Consider (again!) the simplest dynamical model (point-particles in creeping flow) for the simplest non-spherical shape (rod/ellipsoid):

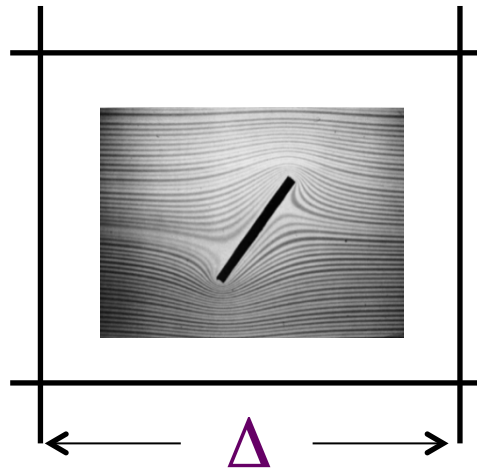


No wake -> Stokes flow

$$\text{Re}_p = \frac{u_{rel} L}{\nu} \ll 1$$

$\lambda = L / D$ Aspect ratio
 θ Orientation

$L, D \ll \eta_K, \Delta \rightarrow$ Pointwise



$$m_p \frac{d\mathbf{v}_p}{dt} = \sum_i \mathbf{F}_i$$

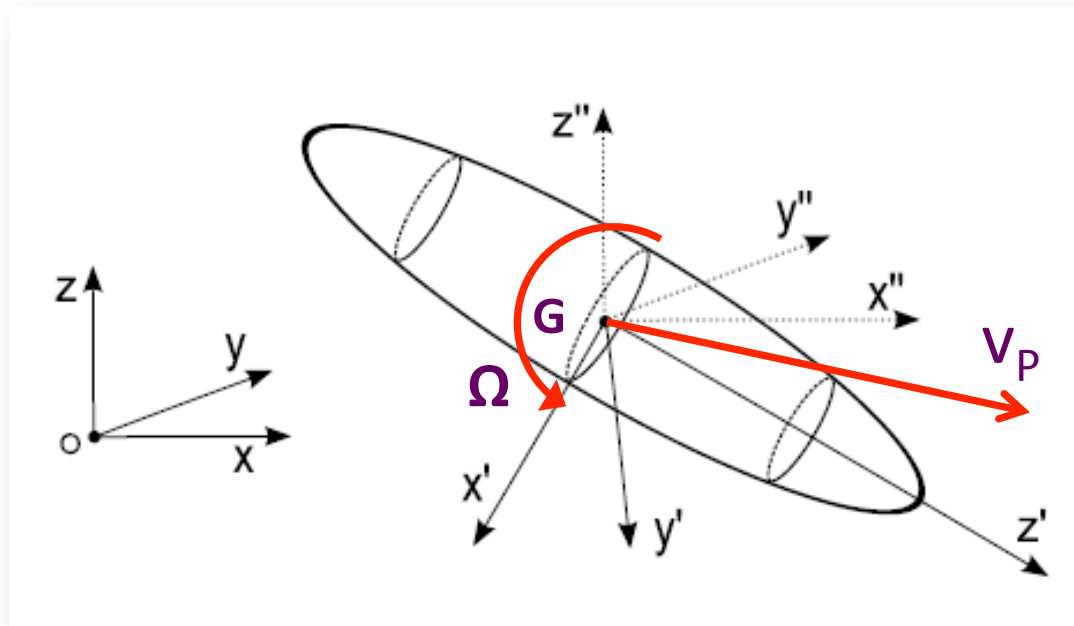
Force model

Drag <- Fluid action
+
Particle orientation

$$C_D = \frac{\mathbf{F}_D}{\frac{1}{2} \rho \mathbf{u}_{rel}^2 A_p} = f(\text{Re}_p, \lambda, \theta)$$

The pointwise approximation for non-spherical particles

The simplest approach to deal with non-spherical particles is to describe their translation and rotation with a “lumped-variable” model



Basically, particle = Lagrangian point moving in 3D space. Finite-size effects neglected!

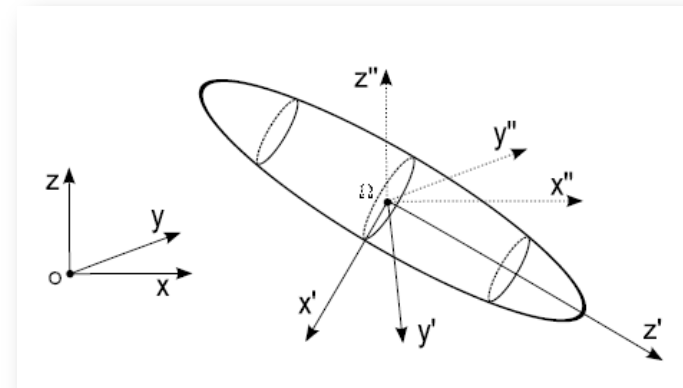
Lagrangian equations of motion for non-spherical particles

- Translational dynamics (enough for a spherical particle)

$$m_p \frac{d\mathbf{v}_p}{dt} = \sum_i \mathbf{F}_i = \mathbf{F}_D + \mathbf{F}_g + \mathbf{F}_L + \mathbf{F}_{PG} + \mathbf{F}_{AM} + \mathbf{F}_B + \dots$$

- Rotational dynamics (needed for a non-spherical particle)

$$\begin{cases} I_x \frac{d\omega_x}{dt} = \sum_i T_{x,i} + \omega_y \omega_z (I_y - I_z) \\ I_y \frac{d\omega_y}{dt} = \sum_i T_{y,i} + \omega_z \omega_x (I_z - I_x) \\ I_z \frac{d\omega_z}{dt} = \sum_i T_{z,i} + \omega_x \omega_y (I_x - I_y) \end{cases}$$



Modelling forces for non-spherical particles

Consider translational dynamics first.

We need force models that account for shape and orientation.

One option is to assume **creeping flow** conditions.

For drag:
(Oberbeck, 1876)

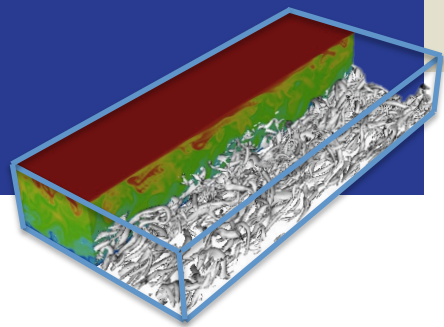
$$\mathbf{f}_\lambda = \frac{\mathbf{F}_D(\lambda, \text{Re}_p \rightarrow 0)}{3\pi d_p \mu_f \mathbf{u}_{\text{rel}}}$$

$$\mathbf{f}_{\lambda\parallel} = \frac{(4/3)\lambda^{-1/3}(1-\lambda^2)}{\lambda - \frac{(2\lambda^2-1)\ln(\lambda + \sqrt{\lambda^2-1})}{\sqrt{\lambda^2-1}}}$$

$$\mathbf{f}_{\lambda\perp} = \frac{(8/3)\lambda^{-1/3}(\lambda^2-1)}{\lambda + \frac{(2\lambda^2-3)\ln(\lambda + \sqrt{\lambda^2-1})}{\sqrt{\lambda^2-1}}}$$

$$\mathbf{F}_D(\lambda, \text{Re}_p \rightarrow 0) = 3\pi d_p \mu_f (\mathbf{u}_{\text{rel}\parallel} \cdot \mathbf{f}_{\lambda\parallel} + \mathbf{u}_{\text{rel}\perp} \cdot \mathbf{f}_{\lambda\perp})$$

Modelling forces for non-spherical particles



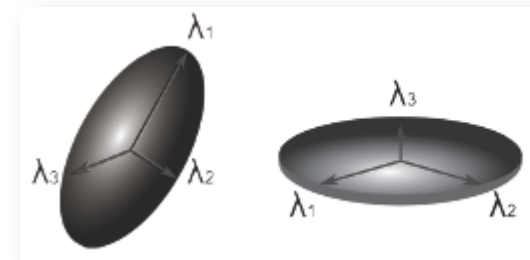
For an ellipsoid:

$$\mathbf{F}_D(\lambda, \text{Re}_p \rightarrow 0) = 3\pi d_p \mu_f (\mathbf{u}_{\text{rel},1} \cdot \mathbf{f}_{\lambda_1} + \mathbf{u}_{\text{rel},2} \cdot \mathbf{f}_{\lambda_2} + \mathbf{u}_{\text{rel},3} \cdot \mathbf{f}_{\lambda_3})$$

For a spheroid: $\mathbf{f}_{\lambda_1} = \mathbf{f}_{\lambda_{\parallel}}$ and $\mathbf{f}_{\lambda_2} = \mathbf{f}_{\lambda_3} = \mathbf{f}_{\lambda_{\perp}}$

Note 1 - minimum drag shape is obtained:

- for a sphere averaging over all orientations
- for a prolate spheroid with $\lambda=1.955$ for stationary orientation (// to symmetry axis)



Note 2 – creeping flow conditions hold if:

$$\mathbf{u}_{\text{rel},1} = \mathbf{u}_{\text{f@p}} - \mathbf{v}_p \cong 0$$

(small slip velocity)

and/or if: $d_p \ll \eta_f$

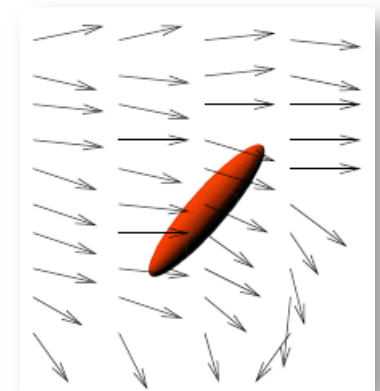
(small particles, yet not Brownian)

Modelling forces for non-spherical particles

Following Bretherton (1962), Brenner (1964, 1965, 1972), Gallily & Cohen (1979):

$$\mathbf{F}_D(\lambda, \text{Re}_p \rightarrow 0) = 6\pi a \mu_f \overline{\mathbf{K}} \cdot (\mathbf{u}_{f@p} - \mathbf{v}_p)$$

with $\overline{\mathbf{K}}$ = translational resistance tensor for arbitrary-shape particle in arbitrary flow field



By analogy, the shear-induced lift force model is:

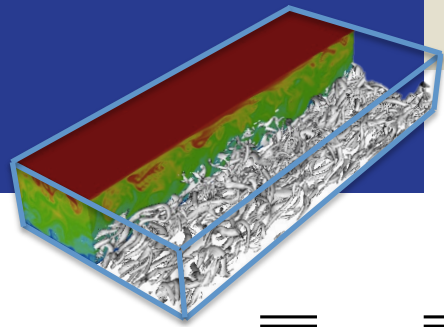
$$C_L = \frac{\mathbf{F}_L(\text{Re}_p \rightarrow 0, \lambda)}{\frac{1}{2} \rho \mathbf{u}_{\text{rel}}^2 \frac{\pi}{4} d_p^2}$$

$$\mathbf{F}_L(\lambda, \text{Re}_p \rightarrow 0) = \frac{\pi^2 \mu_f a^2}{\sqrt{\nu}} \Gamma \cdot \overline{\mathbf{L}} \cdot (\mathbf{u}_{f@p} - \mathbf{v}_p)$$

with:

$$\Gamma = \left(\frac{\partial u_{f@p,i}}{\partial x_j} \right) \cdot \left(\left| \frac{\partial u_{f@p,i}}{\partial x_j} \right| \right)^{-1/2}$$

Modelling forces for non-spherical particles

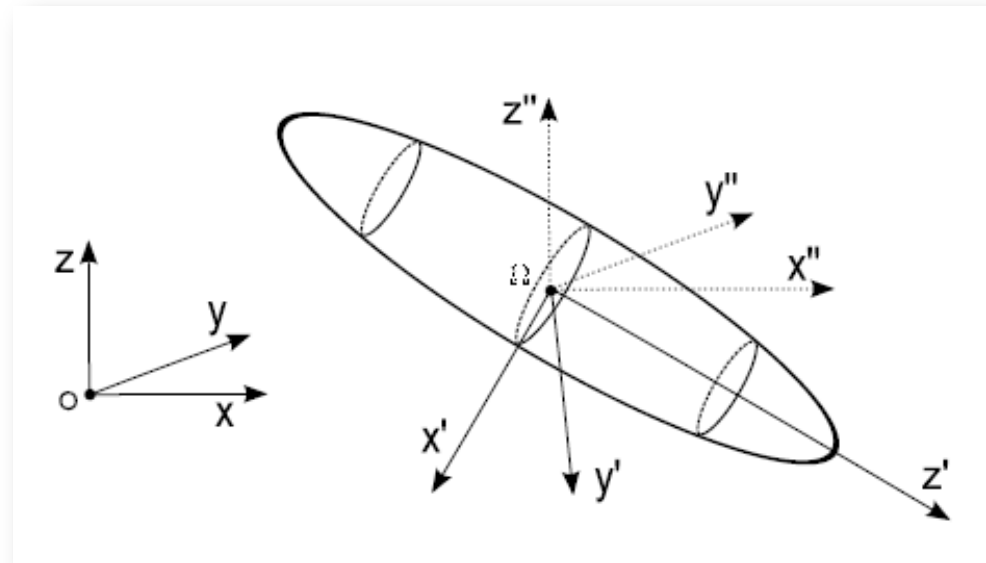


Tensors $\overline{\mathbf{K}}$ and $\overline{\mathbf{L}}$ can be conveniently expressed wrt a frame of reference with:

- origin at the particle center of mass
- axes being the principal axes of the particle

The “usual” approach is to consider:

1. Inertial Frame $X=[x,y,z]$
2. Particle Frame $X'=[x',y',z']$
3. Co-moving frame $X''=[x'',y'',z'']$



Modelling forces for non-spherical particles

In the particle frame:

$$\underline{\underline{\mathbf{K}'}} = \begin{bmatrix} k_{x'x'} & 0 & 0 \\ 0 & k_{y'y'} & 0 \\ 0 & 0 & k_{z'z'} \end{bmatrix}$$

For prolate particles:

$$k_{x'x'} = k_{y'y'} = \frac{(1 - \lambda^2)}{\lambda - \frac{(2\lambda^2 - 1) \ln(\lambda + \sqrt{\lambda^2 - 1})}{\sqrt{\lambda^2 - 1}}}$$

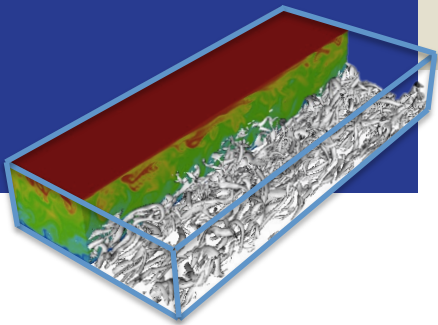
$$k_{z'z'} = \frac{(\lambda^2 - 1)}{\lambda + \frac{(2\lambda^2 - 3) \ln(\lambda + \sqrt{\lambda^2 - 1})}{\sqrt{\lambda^2 - 1}}}$$

See also: Brenner, 1964; Happel & Brenner, 1983

$$\underline{\underline{\mathbf{L}'}} = \begin{bmatrix} 0.0501 & 0.0329 & 0.00 \\ 0.0182 & 0.0173 & 0.00 \\ 0.00 & 0.00 & 0.0373 \end{bmatrix}$$

Note: for a sphere the
original Saffman model
is recovered

Modelling forces for non-spherical particles



In the particle frame:

$$\underline{\underline{\mathbf{K}'}} = \begin{bmatrix} \mathbf{k}_{x'x'} & 0 & 0 \\ 0 & \mathbf{k}_{y'y'} & 0 \\ 0 & 0 & \mathbf{k}_{z'z'} \end{bmatrix}$$

For oblate particles:

$$K'_{xx} = K'_{yy} = \frac{32\pi a(1 - \lambda^2)^{3/2}}{(3 - 2\lambda^2)(\pi - C) - 2\lambda(1 - \lambda^2)^{1/2}}$$

$$K'_{zz} = \frac{16\pi a(1 - \lambda^2)^{3/2}}{(1 - 2\lambda^2)(\pi - C) + 2\lambda(1 - \lambda^2)^{1/2}}$$

See also: Brenner, 1964; Happel & Brenner, 1983

$$\underline{\underline{\mathbf{L}'}} = \begin{bmatrix} 0.0501 & 0.0329 & 0.00 \\ 0.0182 & 0.0173 & 0.00 \\ 0.00 & 0.00 & 0.0373 \end{bmatrix}$$

Note: for a sphere the
original Saffman model
is recovered

Rigid body kinematics

How to go from $\overline{\overline{\mathbf{K}'}}$ to $\overline{\overline{\mathbf{K}}}$?



$$\overline{\overline{\mathbf{K}}}(\varphi, \theta, \psi) = R_{eul}^T \overline{\overline{\mathbf{K}'}} R_{eul}$$

where R_{Eul} = rotation matrix, obtained from the quaternions:

- $e_0 = \cos \left[\frac{1}{2}(\psi + \varphi) \right] \cos \left(\frac{\theta}{2} \right)$
- $e_1 = \cos \left[\frac{1}{2}(\psi - \varphi) \right] \sin \left(\frac{\theta}{2} \right)$
- $e_2 = \sin \left[\frac{1}{2}(\psi - \varphi) \right] \sin \left(\frac{\theta}{2} \right)$
- $e_3 = \sin \left[\frac{1}{2}(\psi + \varphi) \right] \cos \left(\frac{\theta}{2} \right)$
- $e_0^2 + e_1^2 + e_2^2 + e_3^2 = 1$

$$\begin{pmatrix} \dot{e}_0 \\ \dot{e}_1 \\ \dot{e}_2 \\ \dot{e}_3 \end{pmatrix} = \frac{1}{2} \begin{bmatrix} e_0 & -e_1 & -e_2 & e_3 \\ e_1 & e_0 & -e_3 & e_2 \\ e_2 & e_3 & e_0 & -e_1 \\ e_3 & -e_2 & e_1 & e_0 \end{bmatrix} \cdot \begin{pmatrix} 0 \\ \omega_{x'} \\ \omega_{y'} \\ \omega_{z'} \end{pmatrix}$$

$$R_{eul} = \begin{bmatrix} e_0^2 + e_1^2 - e_2^2 - e_3^2 & 2(e_1e_2 + e_0e_3) & 2(e_1e_3 - e_0e_2) \\ 2(e_1e_2 - e_0e_3) & e_0^2 - e_1^2 + e_2^2 - e_3^2 & 2(e_2e_3 + e_0e_1) \\ 2(e_1e_3 + e_0e_2) & 2(e_2e_3 - e_0e_1) & e_0^2 - e_1^2 - e_2^2 + e_3^2 \end{bmatrix}$$

Note: quaternions prevent gimbal lock problems (matrix singularities) but require normalization at each time step

Rigid body kinematics

In summary, compute the resistance tensor in the particle frame as:

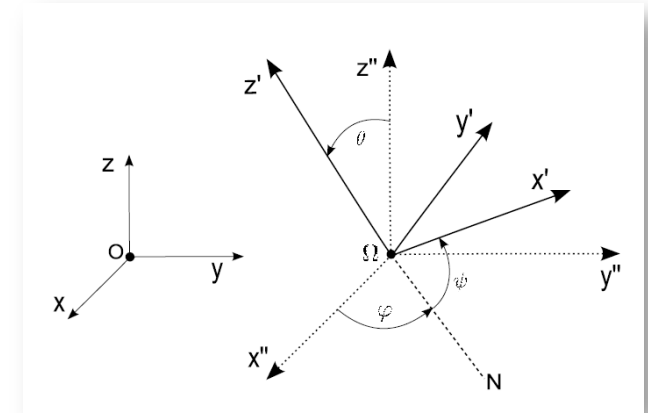
$$\mathbf{F}'_{drag} = \mu\pi a \bar{\bar{\mathbf{K}}}'(\mathbf{u}' - \mathbf{v}')$$

then apply the transformation from the particle frame to the inertial frame:

$$\begin{aligned} \mathbf{F}_{drag} &= R_{eul}^{-1} \mathbf{F}'_{drag} = R_{eul}^T \mathbf{F}'_{drag} = \mu\pi a R_{eul}^T \bar{\bar{\mathbf{K}}}'(\mathbf{u}' - \mathbf{v}') = \\ &= \mu\pi a R_{eul}^T \bar{\bar{\mathbf{K}}}'(R_{eul} \mathbf{u} - R_{eul} \mathbf{v}) = \mu\pi a R_{eul}^T \bar{\bar{\mathbf{K}}}' R_{eul}(\mathbf{u} - \mathbf{v}) \end{aligned}$$

to get:

$$\mathbf{F}_{drag} = \mu\pi a \bar{\bar{\mathbf{K}}}_{(\varphi, \theta, \psi)}(\mathbf{u} - \mathbf{v})$$



Rigid body kinematics

For the lift force (Harper & Chang, JFM,1968; Hogg , JFM, 1994):

$$\mathbf{F}_L = \frac{\pi^2 \mu_f a^2}{\sqrt{\nu}} \Gamma \cdot \left(\overline{\mathbf{K}} \cdot \overline{\mathbf{L}}' \cdot \overline{\mathbf{K}} \right) \cdot \left(\mathbf{u}_{f@p} - \mathbf{v}_p \right)$$

Note that:

- Lift force is non-zero at any non-zero shear rate
- $\mathbf{F}_L \propto a^2$ with a = semi-minor axis -> lift counts for large particles!
- derived for unidirectional shear
- no wall effects included (only available for spheres)
- So far, very little effort done to lift force models for non-spherical particles

“Final” equation of translational motion

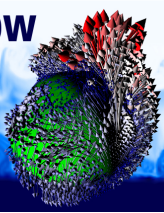
Inertia

Drag

$$m_p \frac{d\mathbf{v}_p}{dt} = \underbrace{\mu_f \pi a \overline{\mathbf{K}}_{(\varphi, \theta, \psi)} \cdot (\mathbf{u}_{f@p} - \mathbf{v}_p)}_{\text{Drag}} +$$

$$+ \underbrace{\frac{\pi^2 \mu_f a^2}{\sqrt{\nu}} \Gamma \cdot (\overline{\mathbf{K}} \cdot \overline{\mathbf{L}}' \cdot \overline{\mathbf{K}})}_{\text{Lift}} \cdot (\mathbf{u}_{f@p} - \mathbf{v}_p) + \underbrace{(m_p - m_f) \mathbf{g}}_{\text{Buoyancy}}$$

plus $\frac{d\mathbf{x}_p}{dt} = \mathbf{v}_p$ to compute particle trajectory



Rotational dynamics

Start from the 2nd cardinal eq. of dynamics in the particle frame:

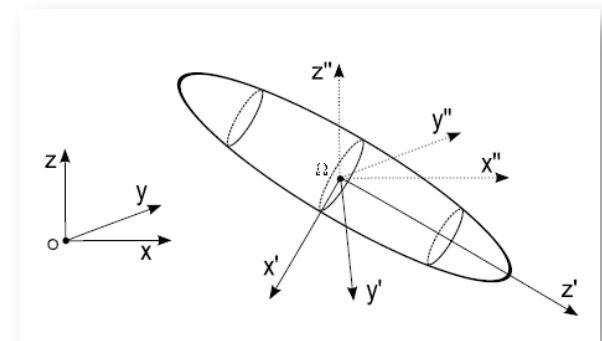
$$\begin{cases} I_{x'x'}\dot{\omega}_{x'} + \omega_{y'}\omega_{z'}(I_{z'z'} - I_{y'y'}) = M_{x'}^{est} \\ I_{y'y'}\dot{\omega}_{y'} + \omega_{x'}\omega_{z'}(I_{z'z'} - I_{x'x'}) = M_{y'}^{est} \\ I_{z'z'}\dot{\omega}_{z'} + \omega_{x'}\omega_{y'}(I_{y'y'} - I_{x'x'}) = M_{z'}^{est} \end{cases}$$

Note - in the particle frame the inertia tensor is constant:

$$I_{x'x'} = I_{y'y'} = \frac{(1 + \lambda^2)a^2}{5} m_P$$

$$I_{z'z'} = \frac{2a^2}{5} m_P .$$

with: $m_p = 4\pi a^3 \lambda \bar{\rho}_p / 3$



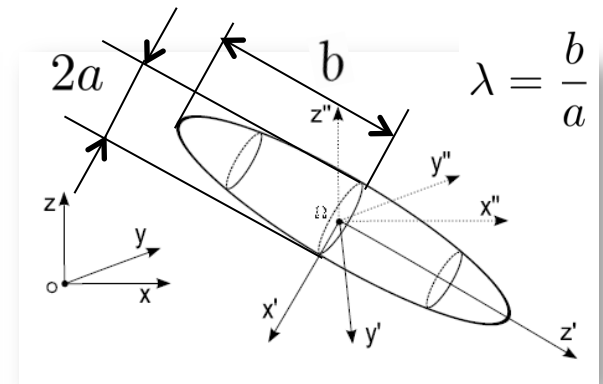
Rotational dynamics

The hydrodynamic torque acting on the particle wrt the principal axes of the particle is computed using Jeffery's formulation (Jeffery, 1922):

$$M_{x'}^{Jeff} = \frac{16\pi\mu a^3\lambda}{3(\beta_0 + \lambda^2\gamma_0)} [(1 - \lambda^2)f' + (1 + \lambda^2)(\xi' - \omega_{x'})]$$

$$M_{y'}^{Jeff} = \frac{16\pi\mu a^3\lambda}{3(\alpha_0 + \lambda^2\gamma_0)} [(\lambda^2 - 1)g' + (1 + \lambda^2)(\eta' - \omega_{y'})]$$

$$M_{z'}^{Jeff} = \frac{32\pi\mu a^3\lambda}{3(\beta_0 + \alpha_0)} (\chi' - \omega_{z'})$$



For prolate spheroids (Gallily & Cohen, 1979):

$$\alpha_0 = \beta_0 = \frac{2\lambda^2\sqrt{\lambda^2 - 1} + \lambda \cdot \ln\left(\frac{\lambda - \sqrt{\lambda^2 - 1}}{\lambda + \sqrt{\lambda^2 - 1}}\right)}{2(\lambda^2 - 1)^{3/2}}$$

$$\gamma_0 = \frac{2\sqrt{\lambda^2 - 1} + \lambda \cdot \ln\left(\frac{\lambda - \sqrt{\lambda^2 - 1}}{\lambda + \sqrt{\lambda^2 - 1}}\right)}{(\lambda^2 - 1)^{3/2}}$$

For oblate spheroids (Siefert et al., 2014):

$$\alpha_0 = \beta_0 = -\frac{\lambda}{2(1 - \lambda^2)^{3/2}} [C - \pi + 2\lambda(1 - \lambda^2)^{1/2}],$$

$$\gamma_0 = \frac{1}{(1 - \lambda^2)^{3/2}} [\lambda C - \lambda\pi + 2(1 - \lambda^2)^{1/2}],$$

$$C = 2 \tan^{-1}(\lambda(1 - \lambda^2)^{-1/2})$$

Rotational dynamics

The hydrodynamic torques depend on the elements of:

- rate of strain tensor:

$$S_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \left\{ \begin{array}{l} f' = \frac{1}{2} \left(\frac{\partial u_{z'}}{\partial y'} + \frac{\partial u_{y'}}{\partial z'} \right) \\ g' = \frac{1}{2} \left(\frac{\partial u_{x'}}{\partial z'} + \frac{\partial u_{z'}}{\partial x'} \right) \end{array} \right.$$

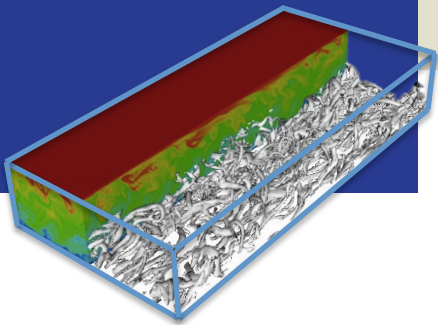
- rate of rotation tensor:

$$\Omega_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right) \left\{ \begin{array}{l} \xi' = \frac{1}{2} \left(\frac{\partial u_{z'}}{\partial y'} - \frac{\partial u_{y'}}{\partial z'} \right) \\ \eta' = \frac{1}{2} \left(\frac{\partial u_{x'}}{\partial z'} - \frac{\partial u_{z'}}{\partial x'} \right) \\ \chi' = \frac{1}{2} \left(\frac{\partial u_{x'}}{\partial y'} - \frac{\partial u_{y'}}{\partial x'} \right) \end{array} \right.$$

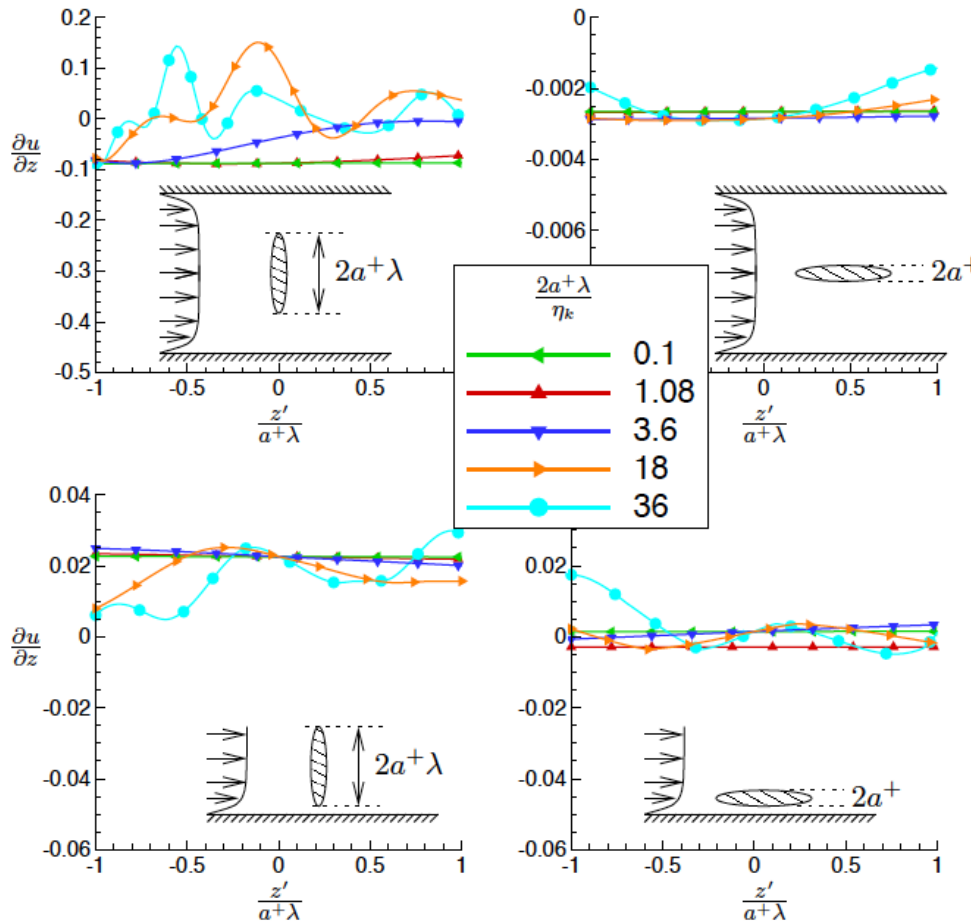
computed in the particle frame: $\bar{\bar{\mathbf{G}}}' = R_{eul} \bar{\bar{\mathbf{G}}} R_{eul}^T$

Rotational dynamics

Caveat: How accurate is Jeffery's formulation?



Channel center...



Near the wall...

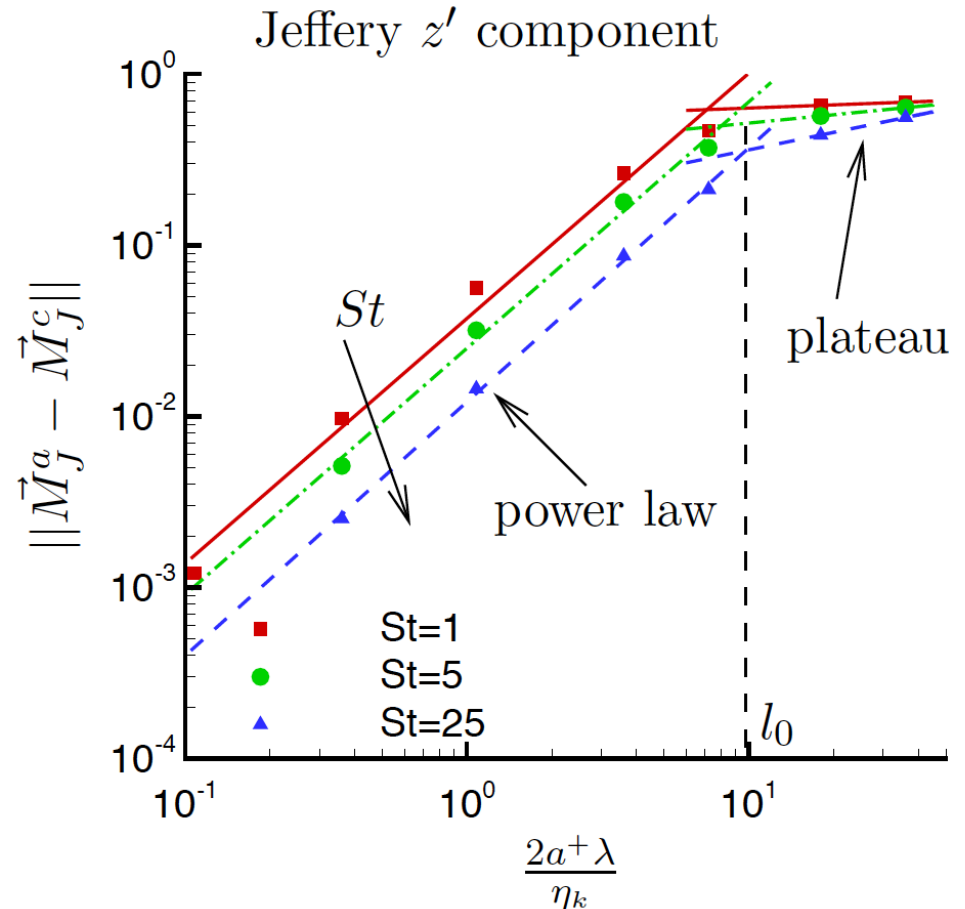
Instantaneous velocity gradient along the ellipsoid at varying aspect ratio

Rotational dynamics

Caveat: How accurate is Jeffery's formulation?

Relative RMS norm:

$$\left\| \vec{M}_J^a - \vec{M}_J^c \right\| = \sqrt{\frac{\sum_i \left(\vec{M}_{J,i}^a - \vec{M}_{J,i}^c \right)^2}{\sum_i \left(\vec{M}_{J,i}^c \right)^2}}$$



Complete system of equations and controlling parameters

Kinematics :

$$\frac{d\mathbf{x}_{(G)}}{dt} = \mathbf{v}$$

$$\dot{e}_0 = \frac{1}{2}(-e_1\omega_{x'} - e_2\omega_{y'} - e_3\omega_{z'})$$

$$\dot{e}_1 = \frac{1}{2}(e_0\omega_{x'} - e_3\omega_{y'} + e_2\omega_{z'})$$

$$\dot{e}_2 = \frac{1}{2}(e_3\omega_{x'} + e_0\omega_{y'} - e_1\omega_{z'})$$

$$\dot{e}_3 = \frac{1}{2}(-e_2\omega_{x'} + e_1\omega_{y'} + e_0\omega_{z'})$$

Dynamics :

$$m_P \frac{d\mathbf{v}}{dt} = (m_P - m_F)\mathbf{g} + \mu \bar{\mathbf{K}}_{(e_0, e_1, e_2, e_3)} \cdot (\mathbf{u} - \mathbf{v})$$

$$I_{x'x'}\dot{\omega}_{x'} + \omega_{y'}\omega_{z'}(I_{z'z'} - I_{y'y'}) = M_{x'}^{Jeff}$$

$$I_{y'y'}\dot{\omega}_{y'} + \omega_{x'}\omega_{z'}(I_{z'z'} - I_{x'x'}) = M_{y'}^{Jeff}$$

$$I_{z'z'}\dot{\omega}_{z'} + \omega_{x'}\omega_{y'}(I_{y'y'} - I_{x'x'}) = M_{z'}^{Jeff}$$

Aspect ratio
(shape)

$$\lambda = \frac{b}{a}$$

Specific density

$$S = \frac{\rho_P}{\rho_F}$$

Response time
(inertia)

$$St = \frac{\tau_P}{\tau_F}$$

It can be anticipated that, in such model, particle behaviour is fully characterized by:

1. Stokes number (incorporates all inertial effects)
2. Aspect ratio (incorporates all shape effects)

Definition of response time for non-spherical particles

Response time for non-spherical particles: how to define it?

For spheres: $St = \frac{2}{9} S(a^+)^2$

For ellipsoids:

- Shapiro & Goldenberg (1993) assumed isotropic particle orientation and used the averaged mobility dyadic (inverse of the translation dyadic)

$$St = \frac{4\lambda Sa^{+2}}{9} \left(\frac{1}{k_{x'x'}} + \frac{1}{k_{y'y'}} + \frac{1}{k_{z'z'}} \right) = \frac{2\lambda Sa^{+2}}{9} \frac{\ln(\lambda + \sqrt{\lambda^2 - 1})}{\sqrt{\lambda^2 - 1}}$$

- Fan & Ahmadi (1995) used the orientation-averaged translation dyadic

$$St = \frac{4\lambda Sa^{+2}}{(k_{x'x'} + k_{y'y'} + k_{z'z'})}$$

Definition of response time for non-spherical particles

For non-spherical particles also the **rotational response time** is important:

For spheres: $St_r = \frac{1}{15} S(a^+)^2 = \frac{3}{10} St$

For ellipsoids no widely-used definition provided so far.
No “unique” expression based on isotropy can be obtained.

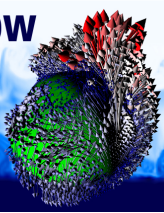
- rotation around z' in the fiber frame:

$$\frac{d\omega_{z'}^+}{dt^+} = \frac{20}{(\alpha_0 + \beta_0)Sa^{+2}} \Delta\omega_{z'}^+ = \frac{1}{\tau_{r,z'}^+} \Delta\omega_{z'}^+ \rightarrow \boxed{\tau_{r,z'}^+ = \frac{\alpha_0 Sa^{+2}}{10}}$$

- rotation around x' or y' in the fiber frame:

$$\frac{d\omega_{y'}^+}{dt^+} = \underbrace{\omega_{x'}^+ \omega_{z'}^+ \left(\frac{2}{1 + \lambda^2} - 1 \right)}_A + \underbrace{\frac{20(\lambda^2 - 1)}{(\alpha_0 + \lambda^2 \gamma_0)(1 + \lambda^2)Sa^{+2}} g'}_B + \underbrace{\frac{20(\lambda^2 + 1)}{(\alpha_0 + \lambda^2 \gamma_0)(1 + \lambda^2)Sa^{+2}} \Delta\omega_{y'}^+}_{1/\tau_{r,y'}}$$

$$\rightarrow \boxed{\tau_{r,y'} = \frac{(\alpha_0 + \lambda^2 \gamma_0)}{20} Sa^{+2} \equiv \tau_{r,x'}}$$



Definition of response time for non-spherical particles

$$\tau_{r,y'} = \frac{(\alpha_0 + \lambda^2 \gamma_0)}{20} Sa^{+2} \equiv \tau_{r,x'}$$

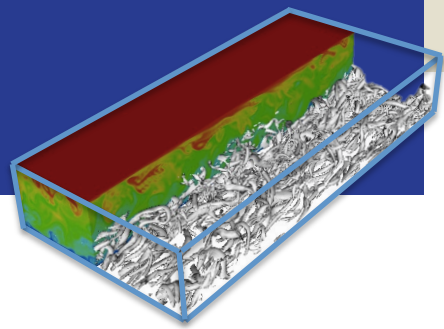
$$\tau_{r,z'}^+ = \frac{\alpha_0 Sa^{+2}}{10}$$

Assume isotropic orientation:

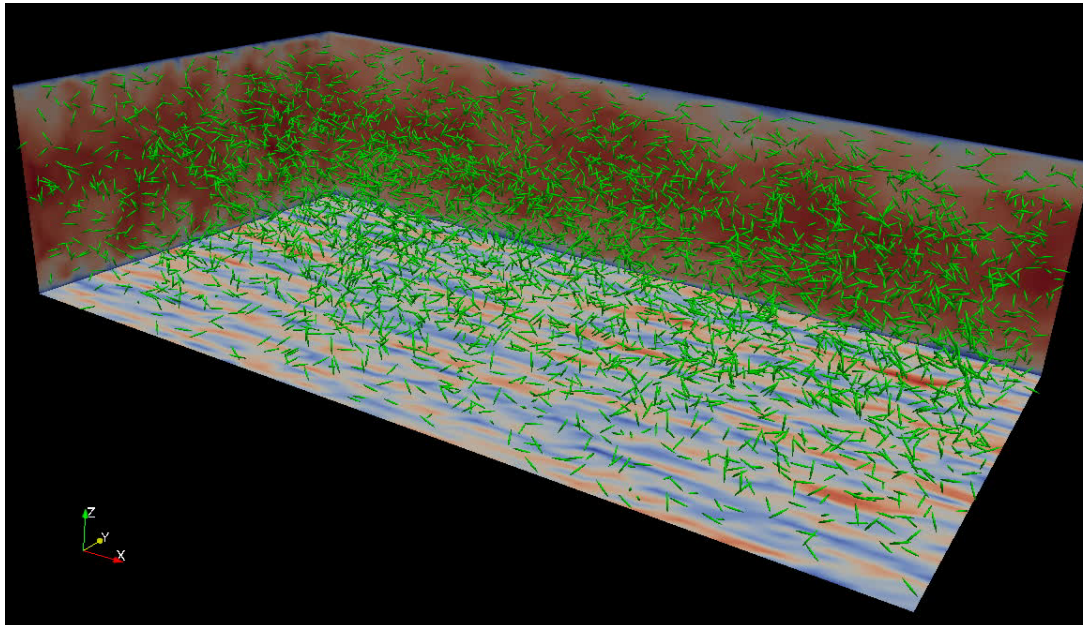
$$\tau_r^+ = \frac{1}{3} (\tau_{r,x'} + \tau_{r,y'} + \tau_{r,z'}) = \frac{2\alpha_0 + \lambda^2 \gamma_0}{30} Sa^{+2} = \frac{3}{10} \tau_p^+ \quad \forall \lambda$$

Example of collective behaviour

Rigid fibers in TCF

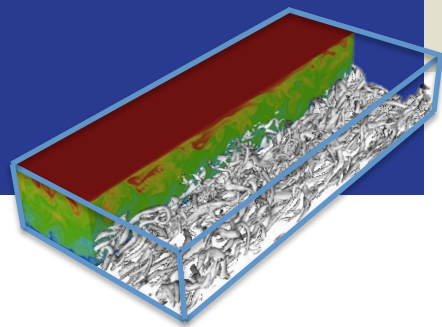


$$\mathbf{x}(t, \lambda), \mathbf{v}(\mathbf{x}(t, \lambda), t, \lambda), \boldsymbol{\omega}(\mathbf{x}(t, \lambda), t, \lambda)$$

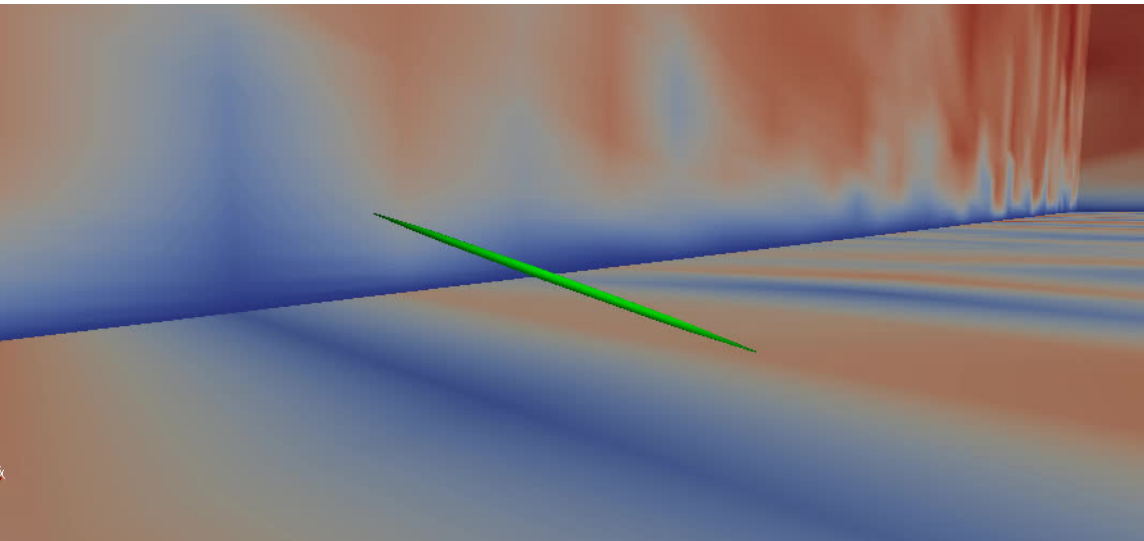


Rigid fibers in TCF

Sources of bias: Inertia + Elongation



Dilute suspension of small rigid fibers in a turbulent channel ($Re_\tau=300$)



Particle functionality added
in the model: **Elongation**

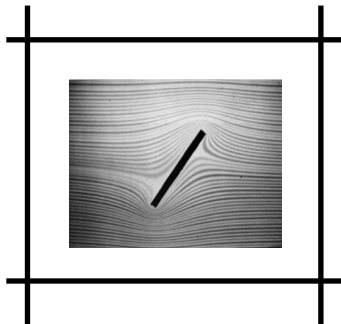
$$\frac{d\mathbf{x}_p}{dt} = \mathbf{v}_p, \quad m_p \frac{d\mathbf{v}_p}{dt} = \sum_i \mathbf{F}_i$$

$$\frac{d(\mathbf{I}\omega_p)}{dt} = \sum_i \mathbf{T}_i$$

$$\mathbf{F}_D = \mu \mathbf{A}^t \mathbf{K}' \mathbf{A} \cdot (\mathbf{u}_f - \mathbf{u}_p)$$

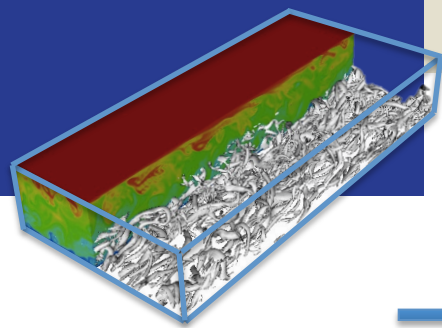
Assumptions:

- fibers = non-interacting ellipsoids with uniform mass distribution in dilute flow
- fiber size < Kolmogorov length scale
- ignore lubrication forces, aggregation/breakage

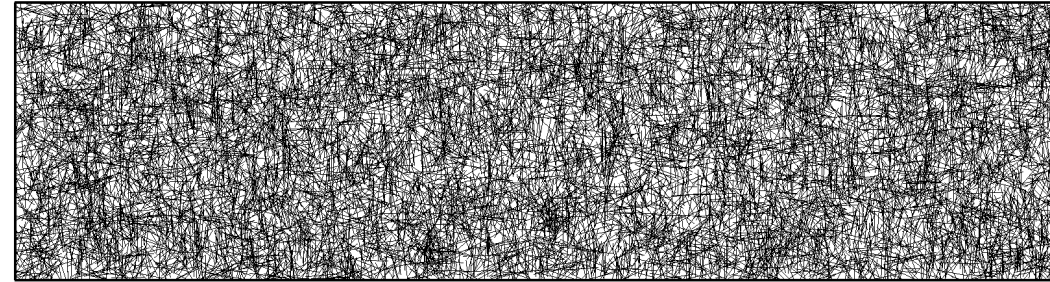


Rigid fibers in TCF

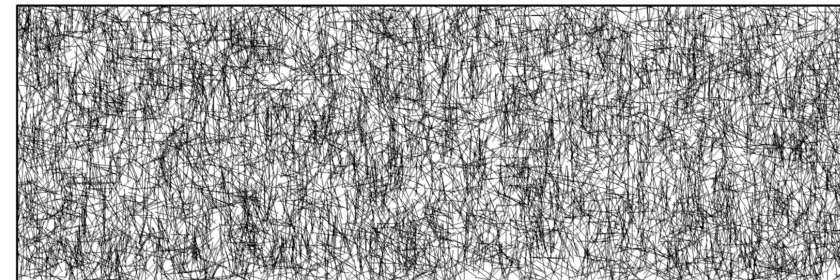
Sources of bias: Inertia + Elongation



Fiber parameters in the animations:
 $St = 30$, $\lambda = 50$, $a^+ = 0.36$

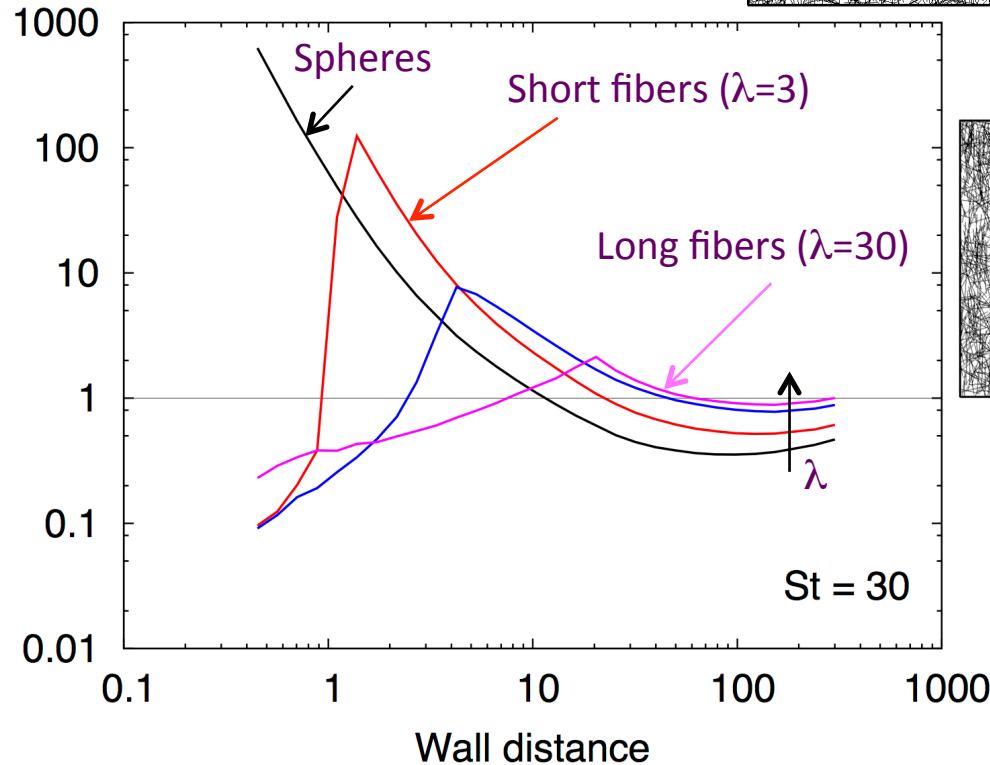


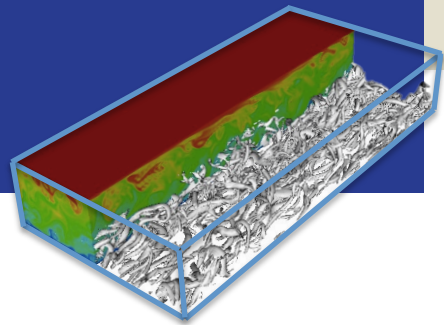
Front view



Side view

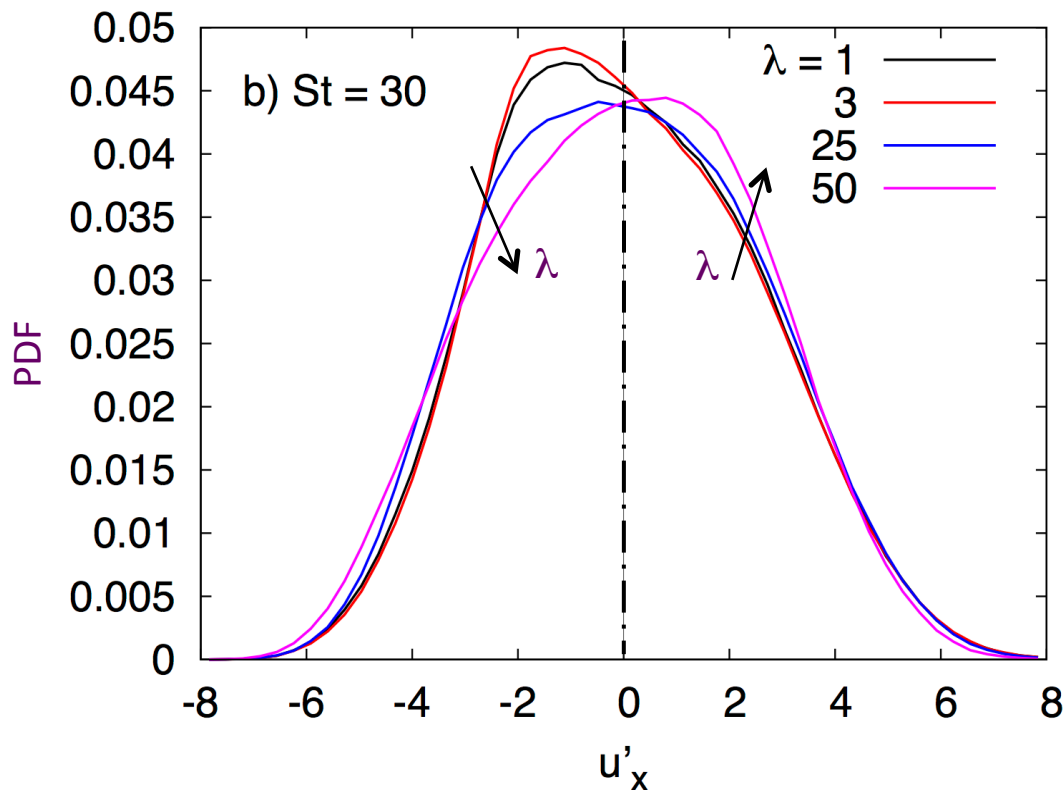
Effect of fiber elongation on near-wall accumulation



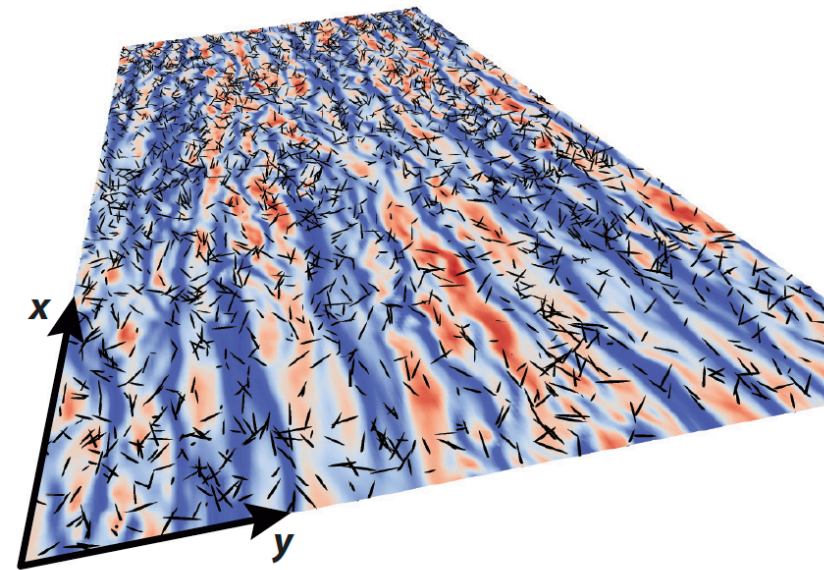


Effect of particle elongation on preferential segregation

Dilute suspension of small rigid fibers in a turbulent channel ($Re_\tau=300$)

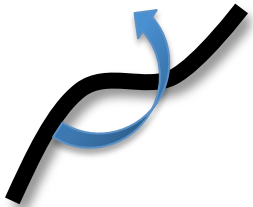
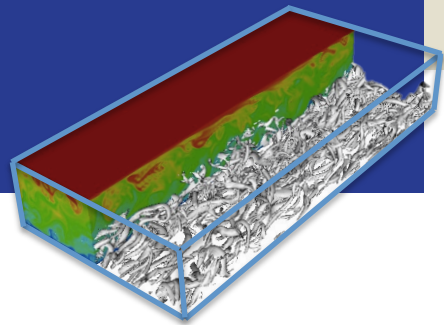


Instantaneous fiber distribution in the near-wall region

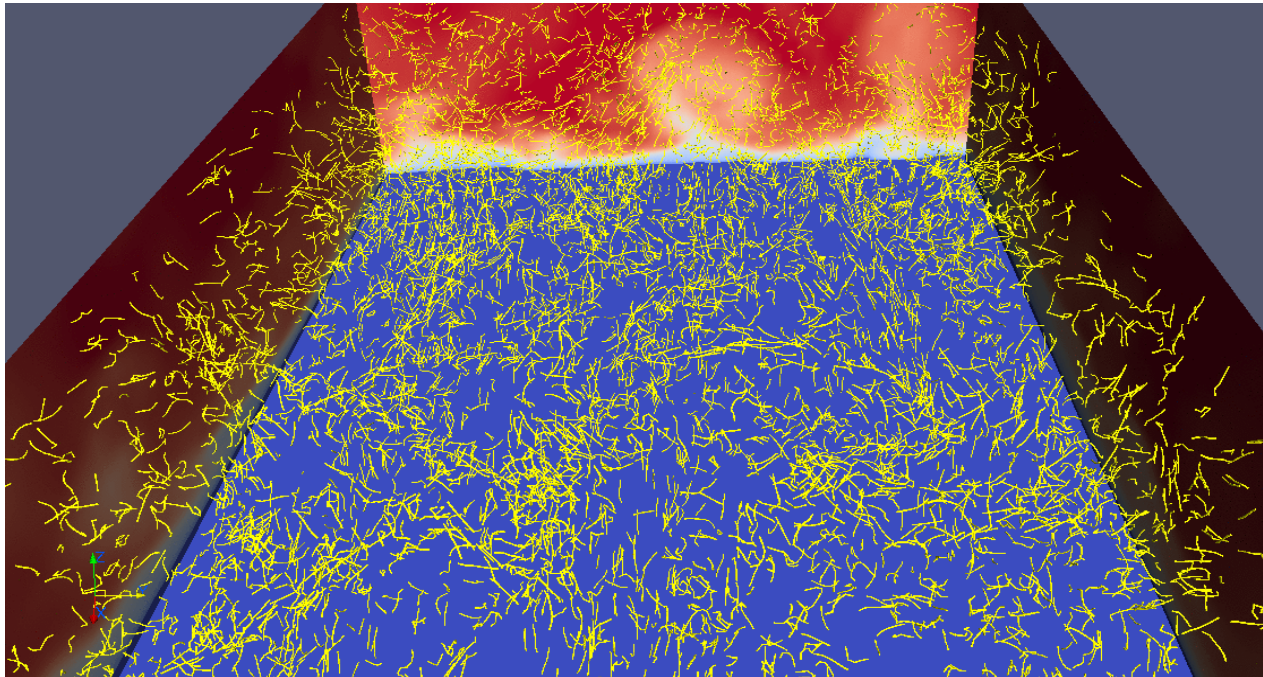


Effect of elongation on near-wall segregation

Example of collective behaviour Flexible fibers in TCF



$$\mathbf{x}(t,\lambda), \mathbf{v}(\mathbf{x}(t,\lambda),t,\lambda), \boldsymbol{\omega}(\mathbf{x}(t,\lambda),t,\lambda), \mathbf{o}(\mathbf{x}(t,\lambda),t,\lambda), \psi(\mathbf{x}(t,\lambda),t,\lambda)$$



Modelling flexibility: How to “mimic” a flexible fiber?

Rod model: flexible fiber = chain of segments/spheres connected by ball-and-socket joints (Delmotte et al '15; Andric et al '13; Slowicka et al '13; Derksen '10; Lindstrom & Uesaka '07)

- Solve for Euler's 1st and 2nd law for each segment:

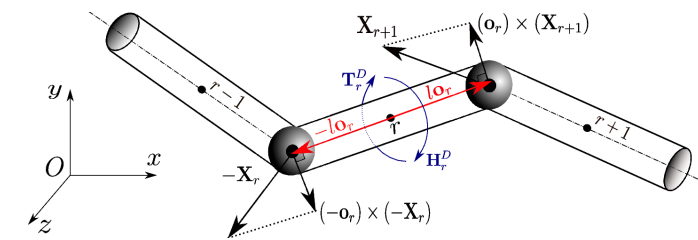
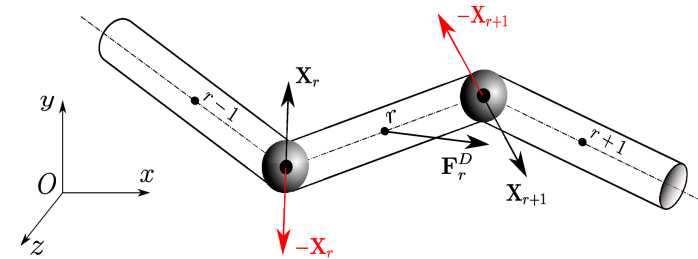
$$m_p \frac{d\mathbf{v}_r}{dt} = \mathbf{F}_r^D + (\mathbf{X}_{r+1} - \mathbf{X}_r)$$

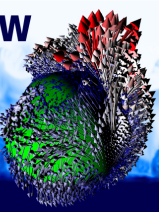
$$\frac{d(\bar{\mathbf{J}}_r \boldsymbol{\omega}_r)}{dt} = \mathbf{T}_r^D + \mathbf{H}_r^D + l \mathbf{o}_r \times (\mathbf{X}_{r+1} + \mathbf{X}_r) + (\mathbf{Y}_{r+1}^b - \mathbf{Y}_r^b)$$

- Impose connectivity constraints between segments:

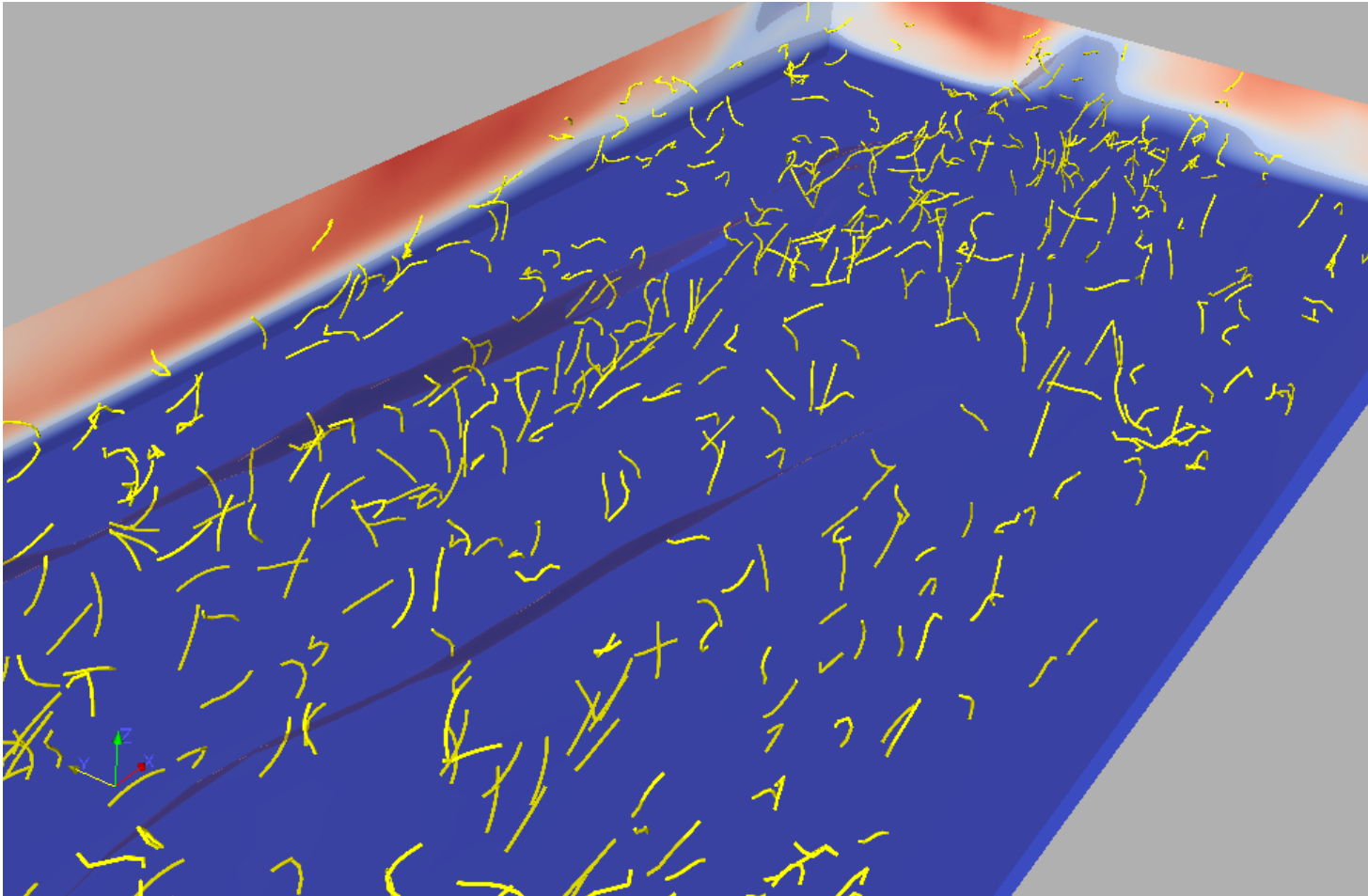
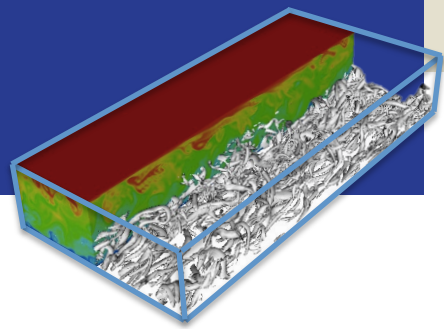
$$\left\{ \begin{array}{l} \frac{\partial \Psi_r}{\partial t} = \mathbf{v}_{r+1} - \mathbf{v}_r + \lambda a (\boldsymbol{\omega}_r \times \mathbf{o}_r + \boldsymbol{\omega}_{r+1} \times \mathbf{o}_{r+1}) = \mathbf{0} \\ \Psi_r|_{t=0} = \mathbf{0} \end{array} \right.$$

$$\Psi_r = \mathbf{p}_r + l \mathbf{o}_r - (\mathbf{p}_{r+1} - l \mathbf{o}_{r+1}) = \mathbf{0}$$



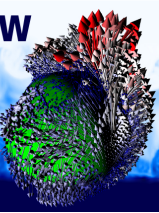


Near-wall accumulation of flexible fibers in turbulent channel flow

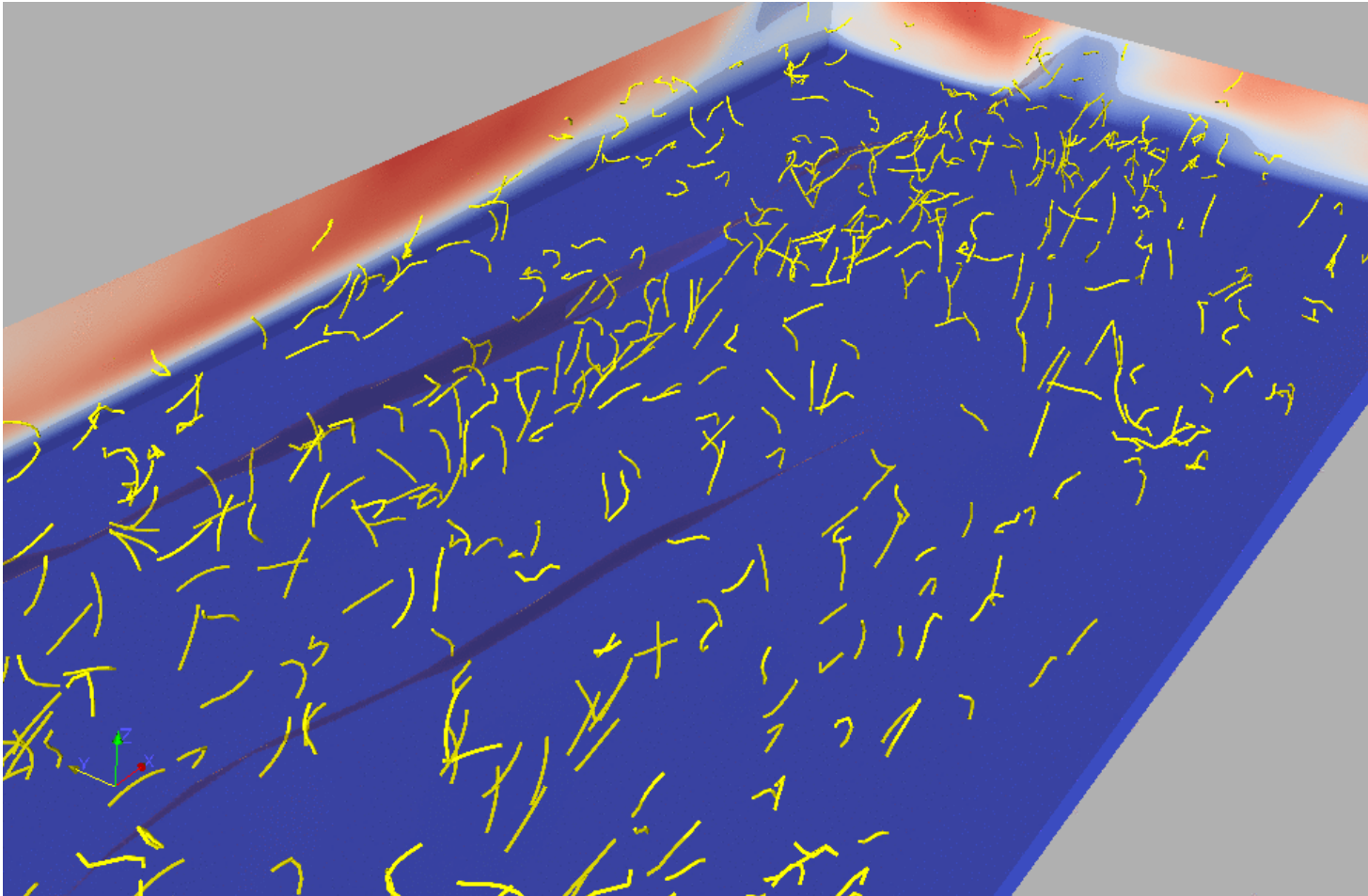
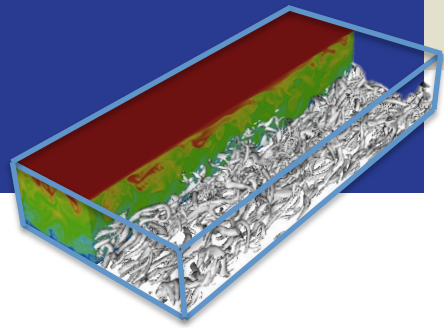


Dilute suspension of small flexible fibers in turbulent channel flow

- Shear Reynolds number: $Re_\tau=150$
- Segment Stokes number: $St_s=5, 30$
- Segment aspect ratio: $\lambda=5$
- Number of segments: 7
- Number of fibers: 200,000



Near-wall accumulation of flexible fibers in turbulent channel flow

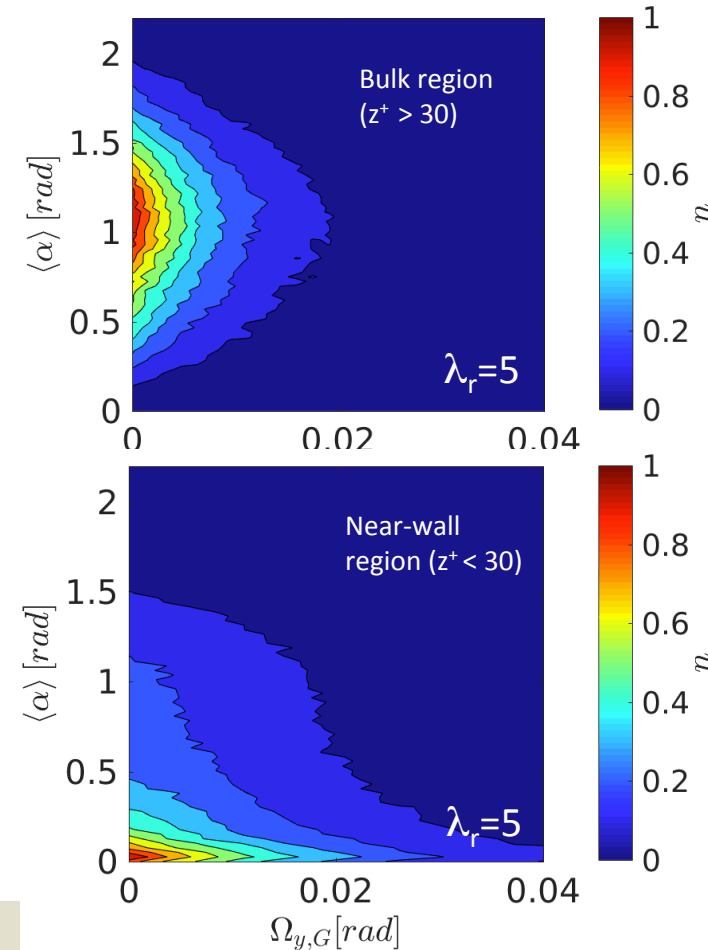
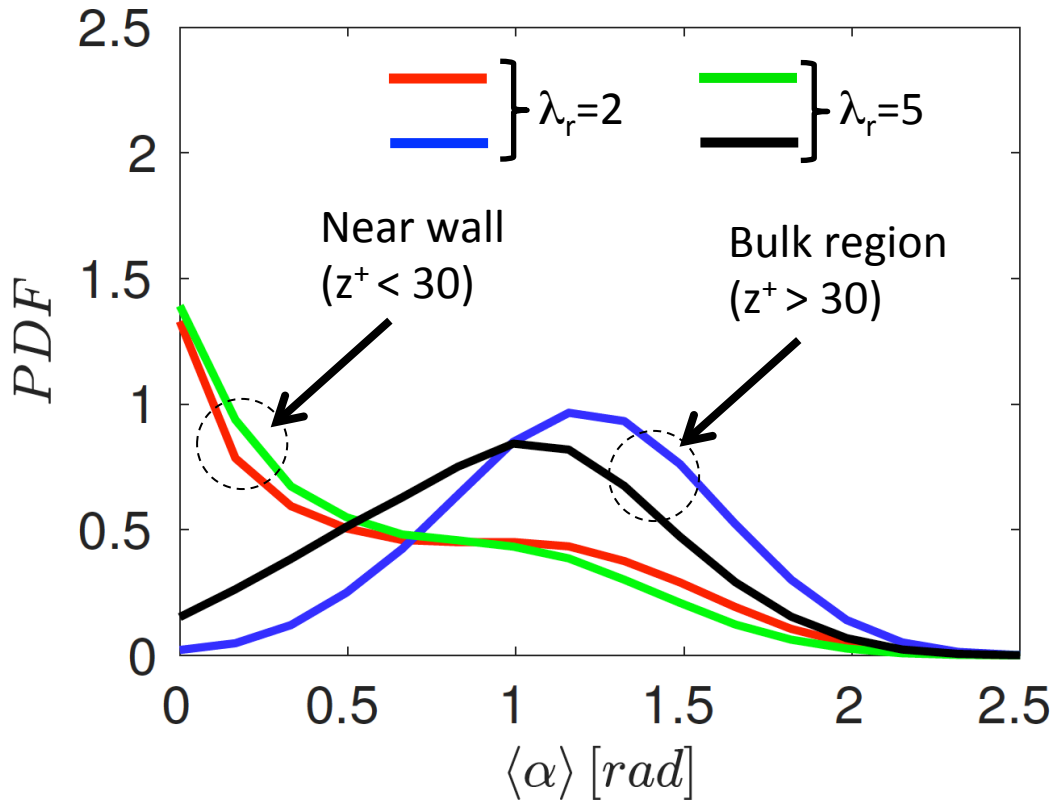


Dilute suspension of small flexible fibers in turbulent channel flow

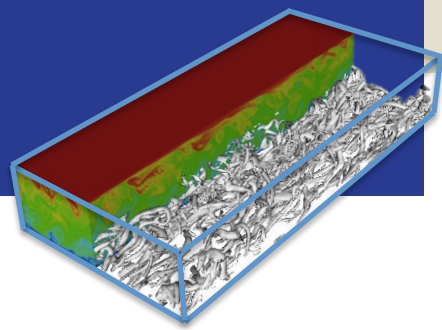
- Shear Reynolds number: $Re_\tau=150$
- Segment Stokes number: $St_s=5, 30$
- Segment aspect ratio: $\lambda=5$
- Number of segments: 7
- Number of fibers: 200,000

Near-wall accumulation of flexible fibers in turbulent channel flow

Effect of flexibility on near-wall segregation (for $St_5=30$)

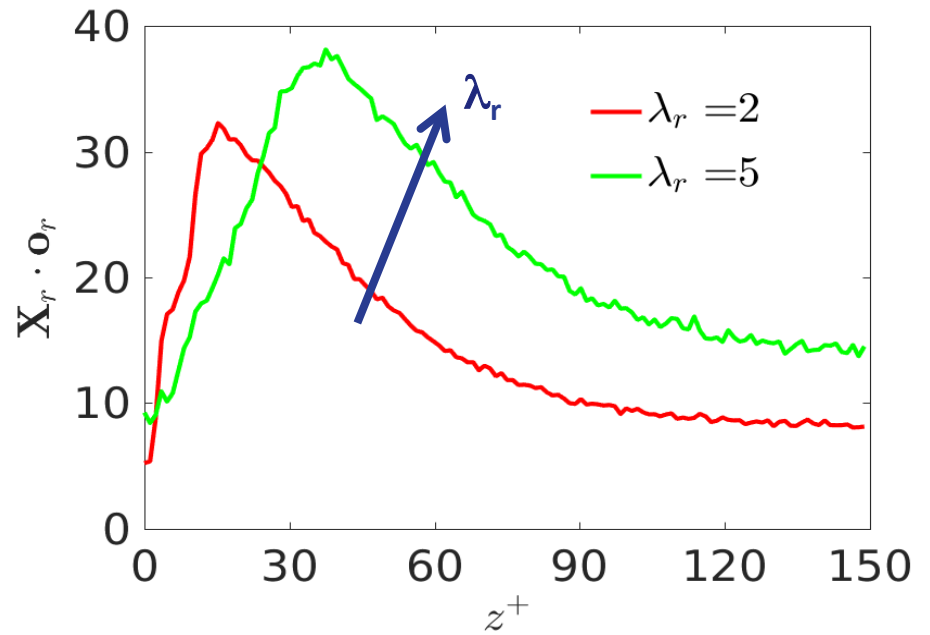
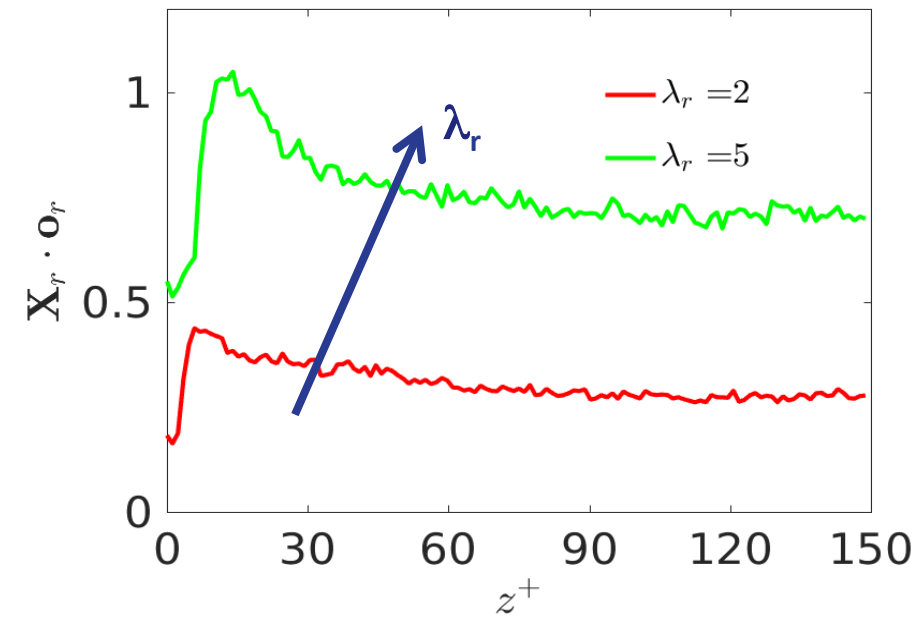


Constraint force acting on fiber elements (along element's axis)



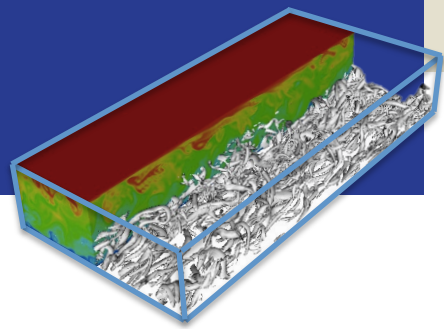
$St_r = 1$

$St_r = 30$



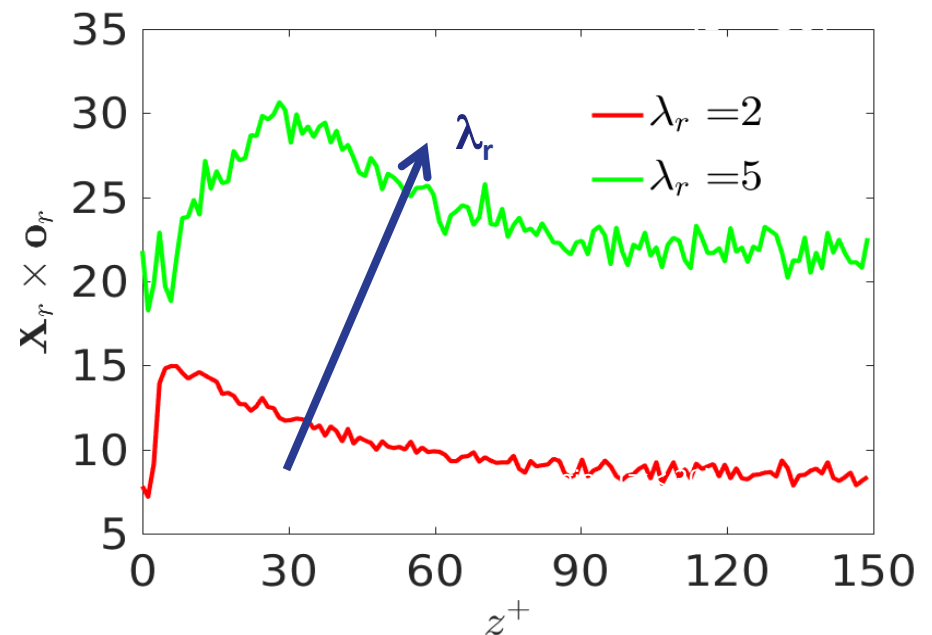
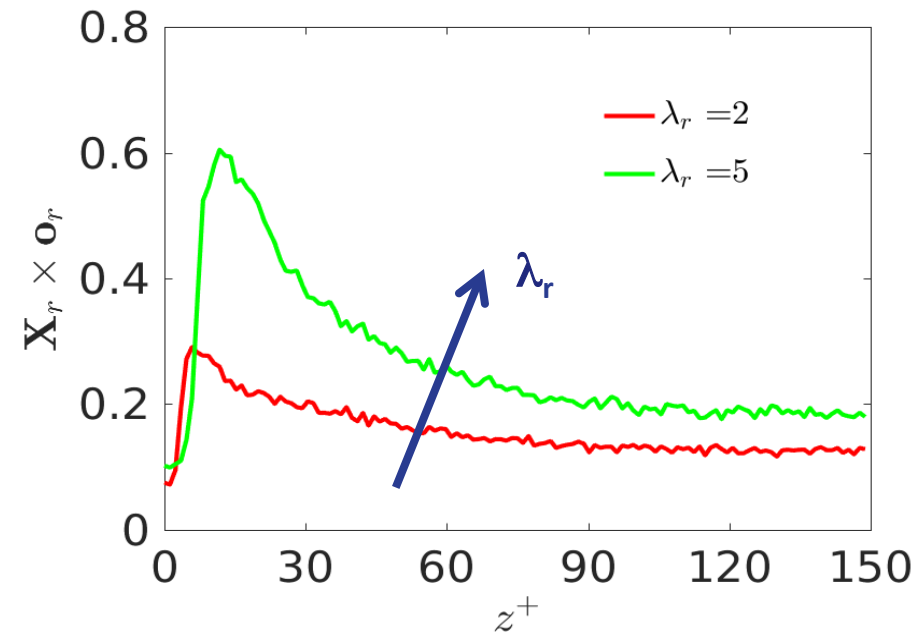
Tensile constraint force as a function of the wall-normal flow direction

Constraint force acting on fiber elements (perpto element's axis)

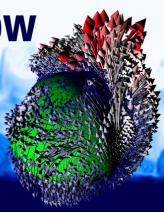


$St_r = 1$

$St_r = 30$



Bending constraint force along the wall-normal flow direction



Lessons learned

- L1. A Lagrangian framework for numerical simulation of spherical/non-spherical particles dynamics (in dilute flow conditions) has been presented
- L2. Equations for particle translation and rotation were derived for particles with arbitrary shape in the Stokes regime (creeping flow)
- L3. The resulting lumped-parameter model provides strong mathematical coupling between translation and rotation (drag and lift depend on particle orientation)
- L4. Particle rotation can be conveniently described using the quaternion formalism
- L5. Equations yield accurate results if particles are small (limit on aspect ratio) and/or have small slip velocity
- L6. Many modelling issues remain open (force models, force coupling schemes, torque coupling schemes, collisions, ...)