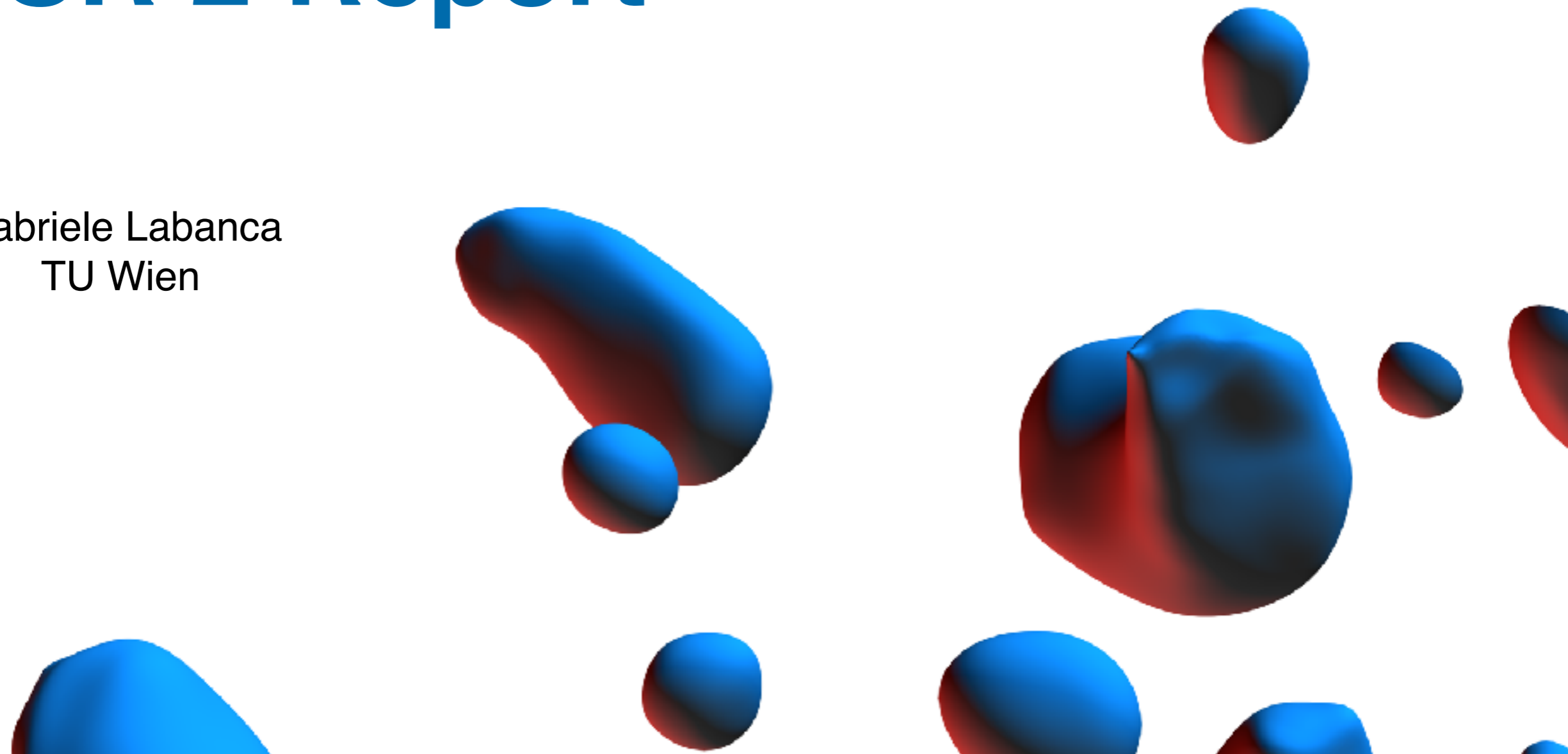


ESR 2 Report

Gabriele Labanca
TU Wien

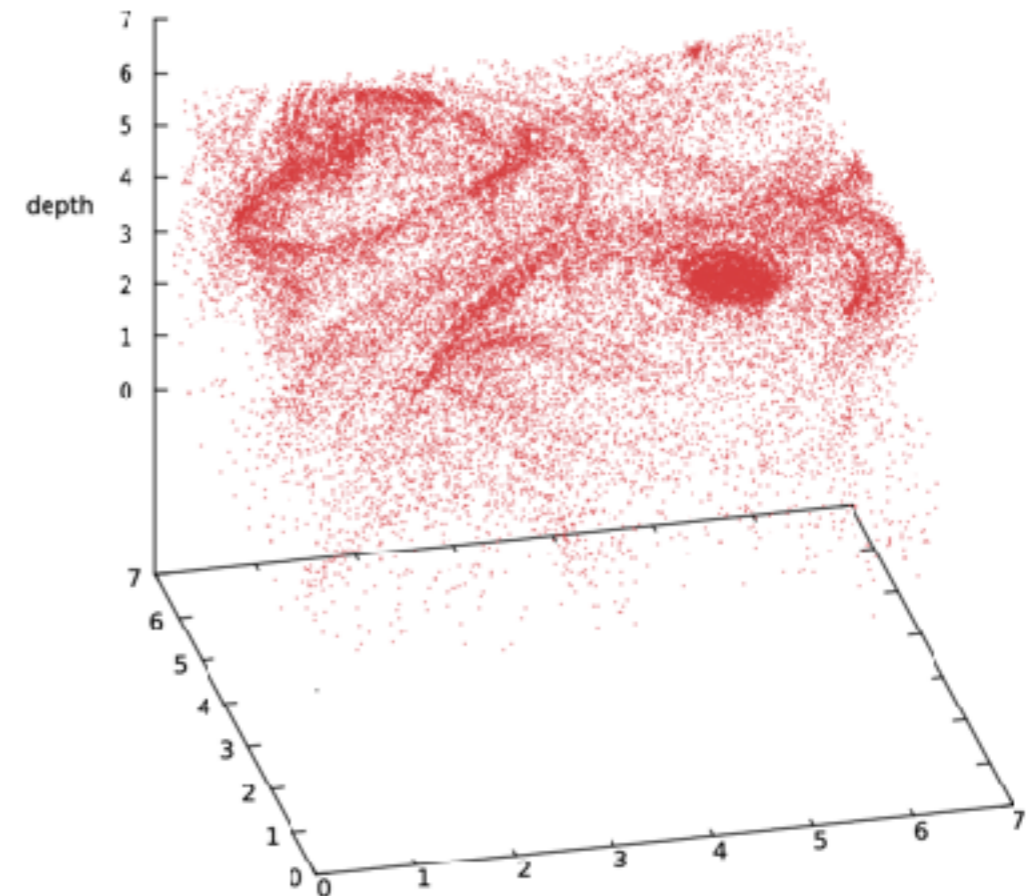


Degree in Physics Bachelor's (Padova) and Master's (Torino)

Study of **Plankton** spatial
distribution in turbulence

$$\partial_t n + v \partial_z n = D \partial_z^2 n + (\lambda f - \mu) n$$

Pseudo-spectral, parallel,
Lagrangian code



Bologna, CINECA, Debugging and Optimisation in High Performance Computing

Vienna, VSC, Parallelisation with MPI; Shared memory parallelisation with OpenMP

Udine, CISM, Advances in Dispersed Multi-Phase Flows: from Measuring to Modeling

Bologna, CINECA, Advanced school on parallel computing (February)

University of Innsbruck, GPU programming with CUDA (March)

<http://www.hpc.cineca.it/news/marconi100-new-accelerated-gpu-cluster>

Chicago, Argonne National Laboratory,

Training program on extreme-scale computing (July)

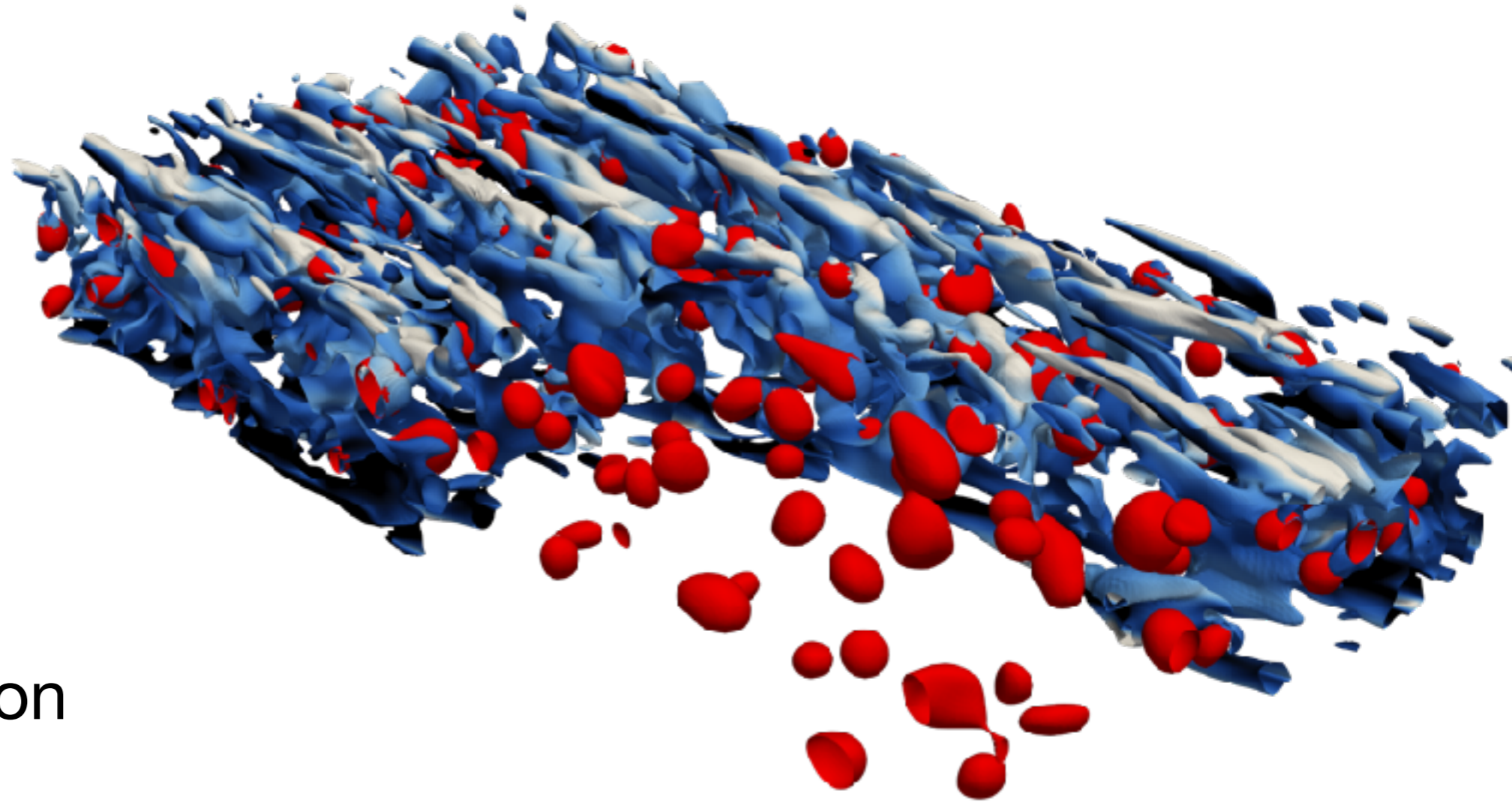
Torino, ETC, Attendance and staff

Vienna, ERCOFTAC, Phase Field simulations of turbulent bubbly flows

Seattle, American Physical Society meeting, Fluid-dynamics division,
Dynamics of large and deformable bubbles in turbulence

Turbulence

$$Re_{\tau} = \frac{\rho_c u_{\tau} h}{\eta_c}$$



Surface tension

Weber number

(ratio between inertial
and surface forces)

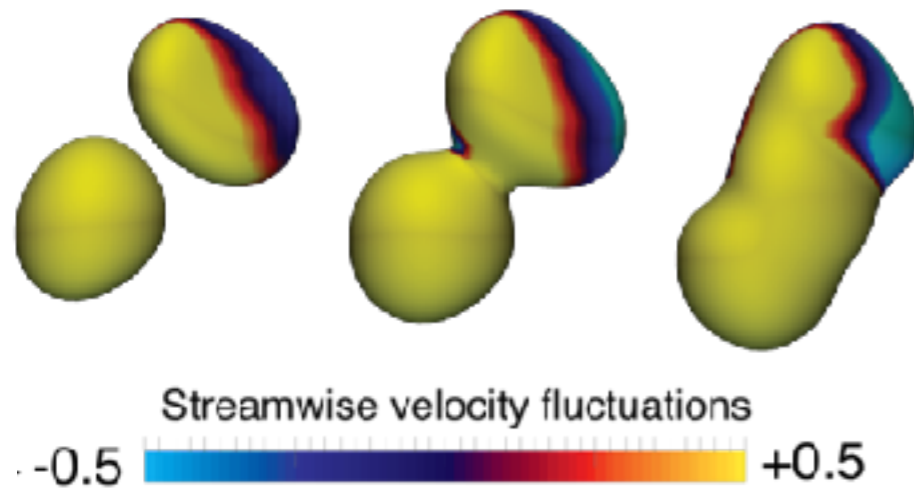
$$We = \frac{\rho_c u_{\tau}^2 h}{\sigma}$$

Viscosity ratio

$$\lambda = \frac{\eta_d}{\eta_c}$$

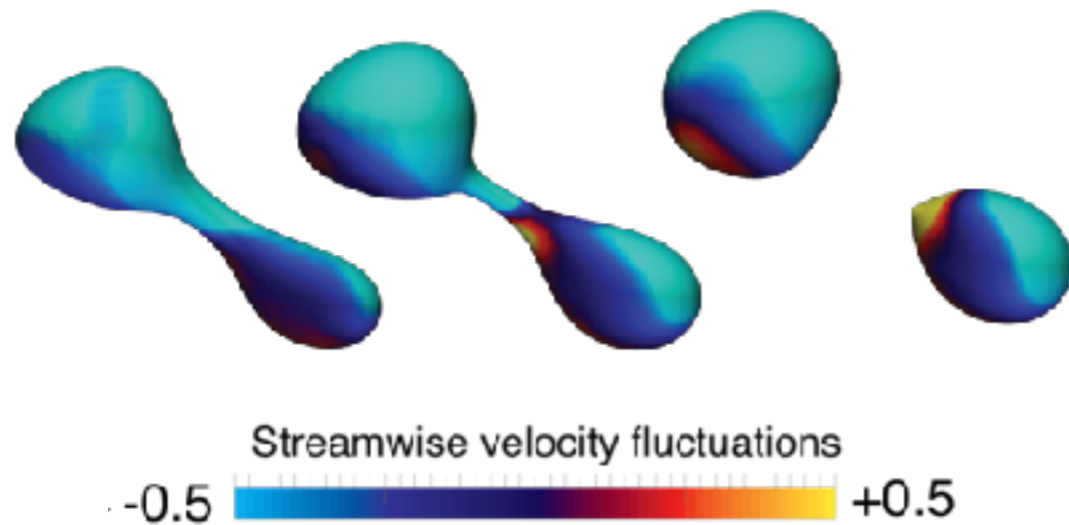
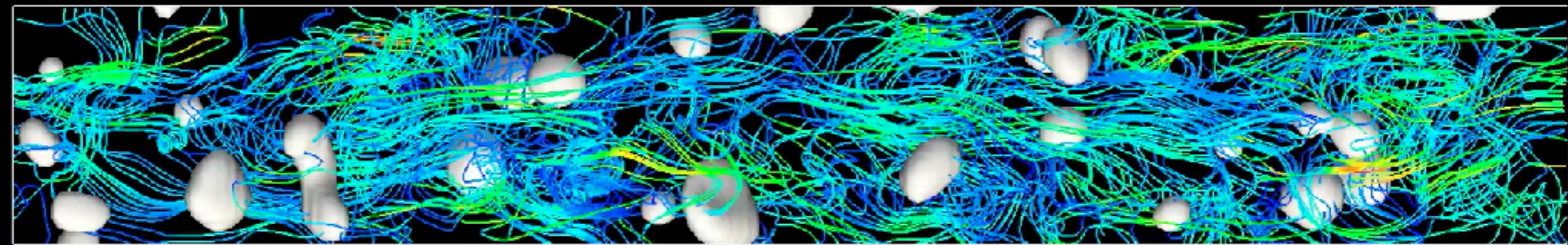
Density ratio

$$\gamma = \frac{\rho_d}{\rho_c}$$



COALESCENCE

Two drops come close and collide due to turbulence fluctuations. During the collision, a small bridge is initially formed; later, surface tension (which tends to reshape the drop) comes into the picture and complete the coalescence process.



BREAK-UP

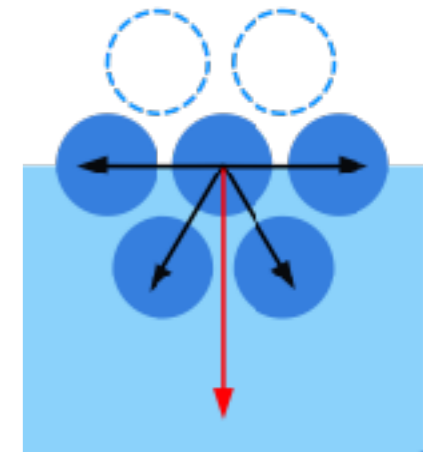
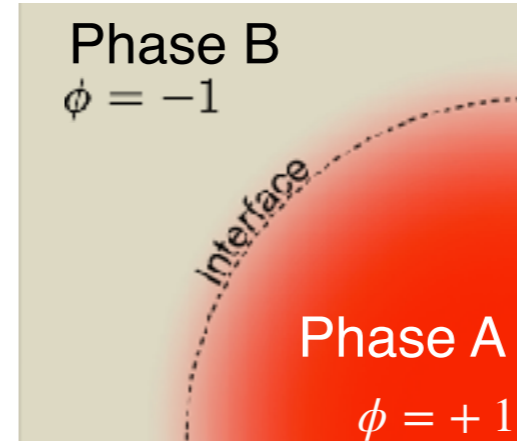
A drop is subjected to a sufficient shear stress, such that it is deformed and stretched until the emerging thin liquid bridge is broken (due to surface tension that acts minimising the energy stored at the interface).

Interface



Cahn-Hilliard

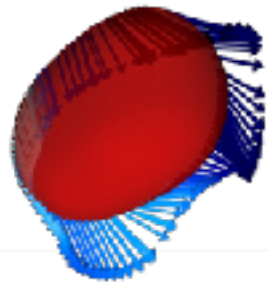
$$\frac{\partial \phi}{\partial t} + \mathbf{u} \cdot \nabla \phi = \frac{1}{Pe_\phi} \nabla^2 \mu_\phi$$



Interface forces
(Korteweg tensor)



Flow



Continuity

$$\nabla \cdot \mathbf{u} = 0$$

Navier-Stokes

$$\rho(\phi) \left[\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right] = -\nabla P + \frac{1}{Re_\tau} \nabla \cdot \left[\eta(\phi) \left(\nabla \mathbf{u} + \nabla \mathbf{u}^T \right) \right] + \frac{3}{\sqrt{8}} \frac{Ch}{We} \nabla \cdot \boldsymbol{\tau}_c$$

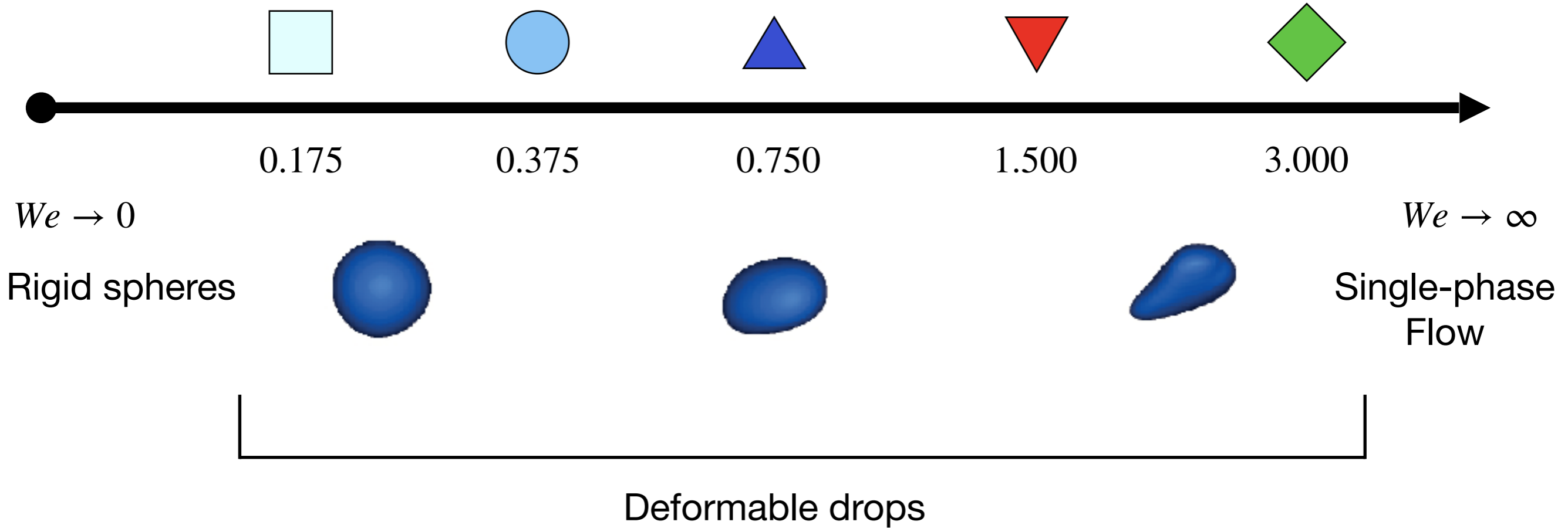
$$\text{Density: } \rho(\phi) = \left[1 + \frac{\gamma - 1}{2} (\phi + 1) \right]$$

$$\text{Viscosity: } \eta(\phi) = \left[1 + \frac{\lambda - 1}{2} (\phi + 1) \right]$$

Effect of Weber number

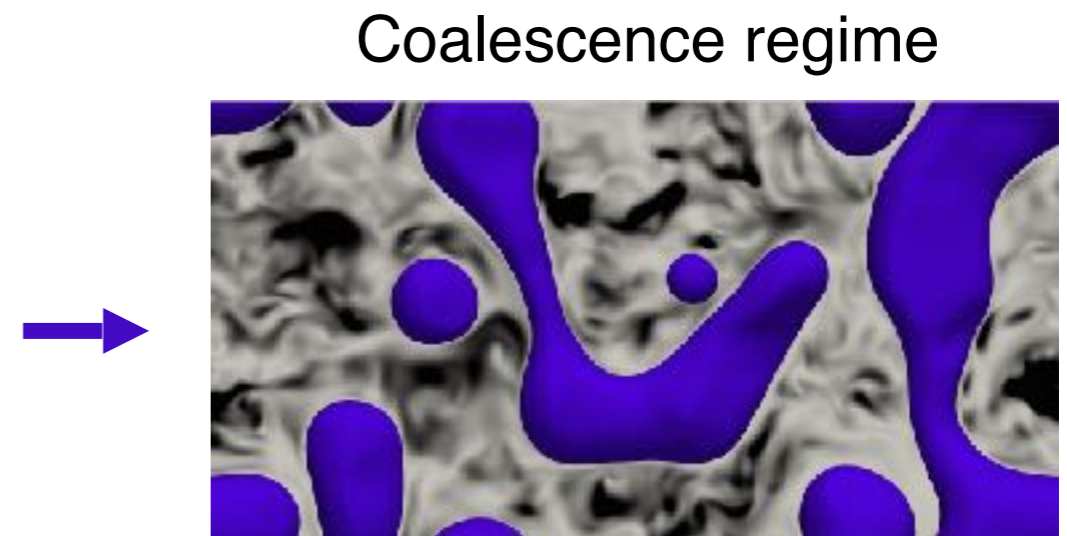
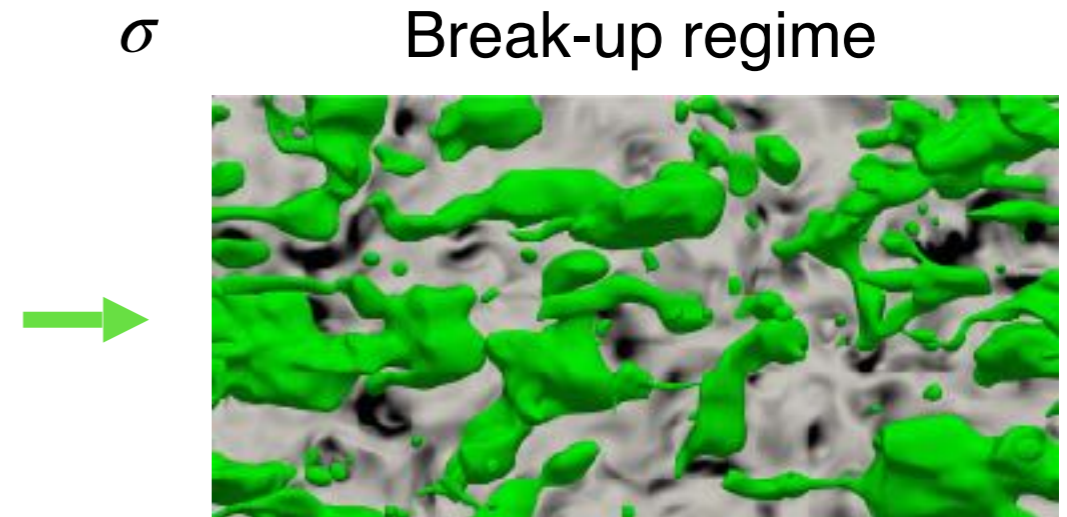
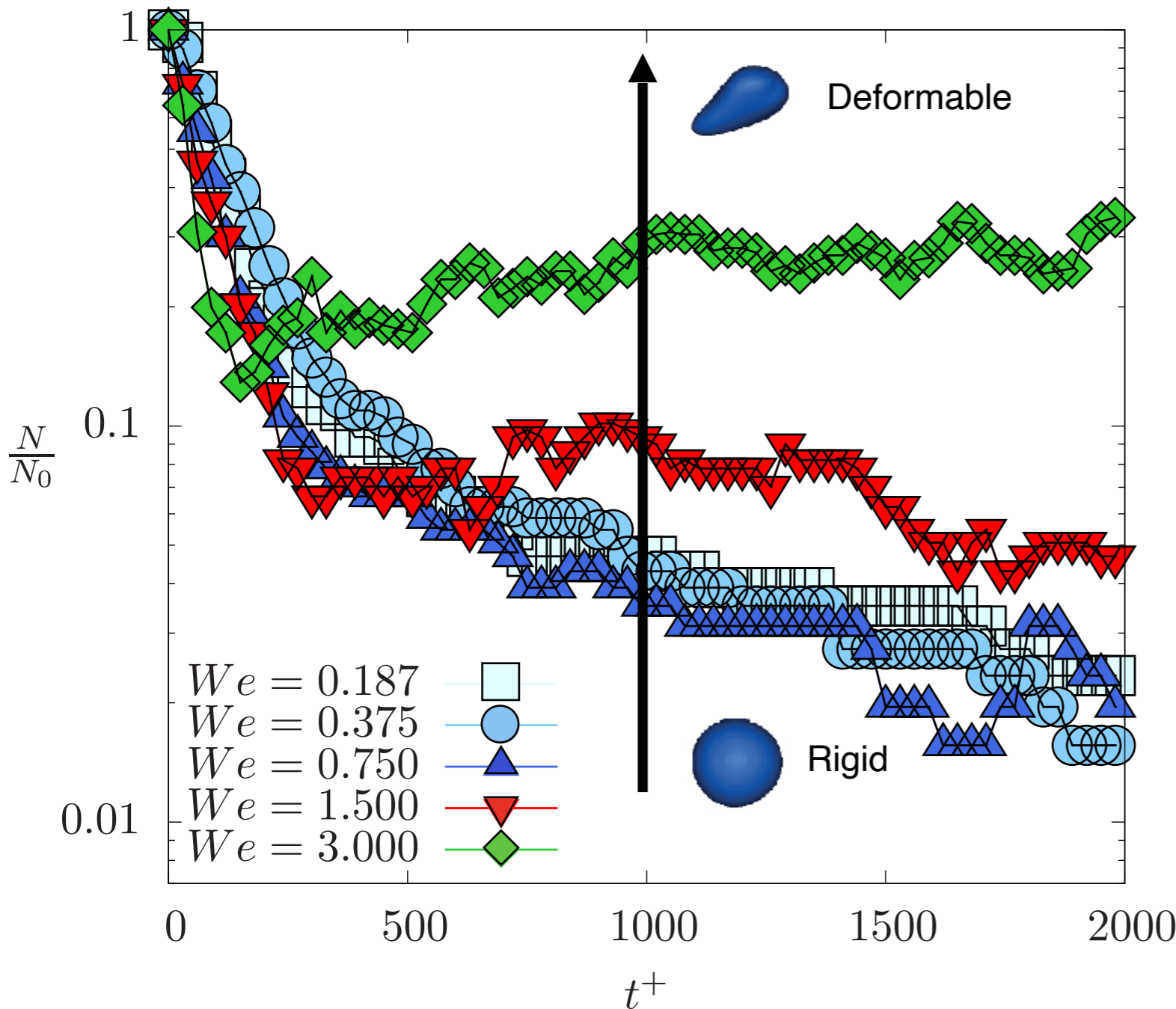
Weber number
(ratio between inertial
and surface forces)

$$We = \frac{\rho_c u_\tau^2 h}{\sigma}$$



Temporal evolution of the number of drops

$$We = \frac{\rho_c u_\tau^2 h}{\sigma}$$



Effect of viscosity ratio and Weber number



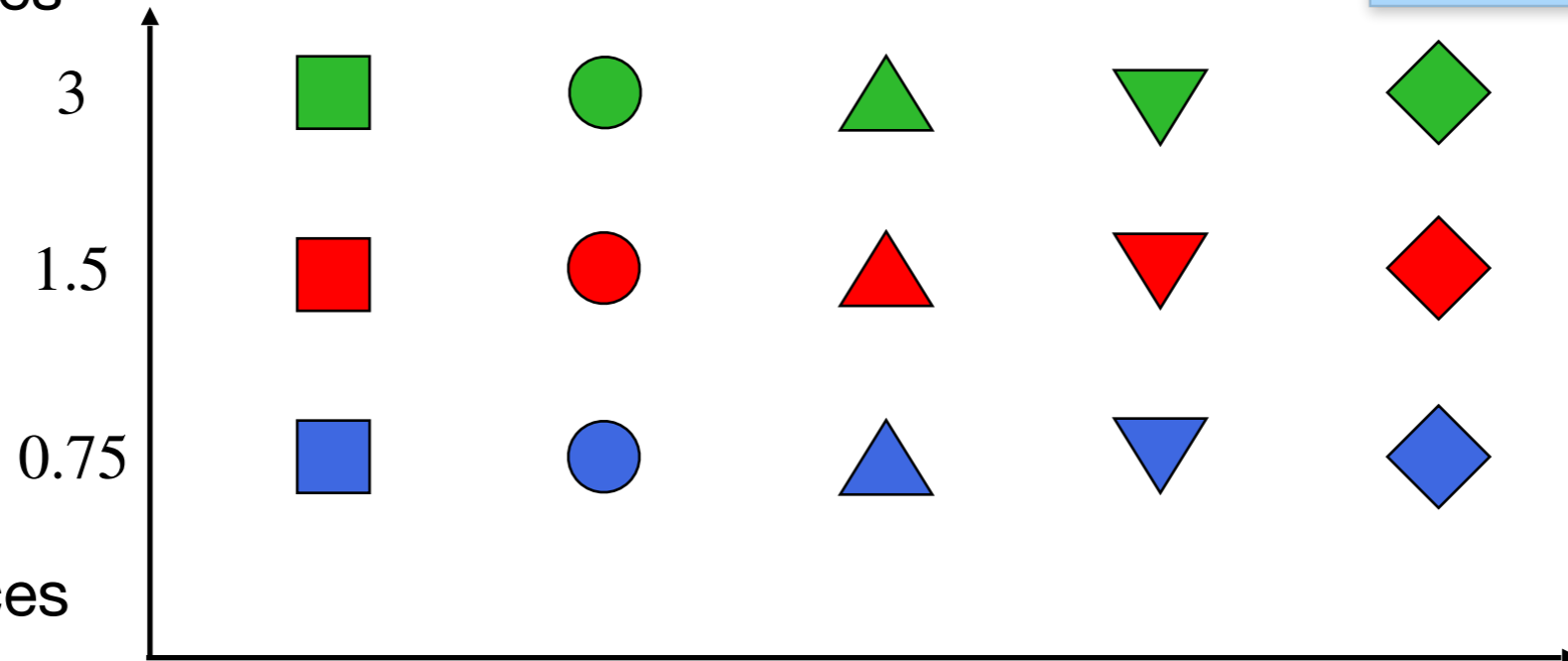
Low surface forces

More viscous droplets dissipate more effectively the turbulence fluctuations.

High surface forces



We



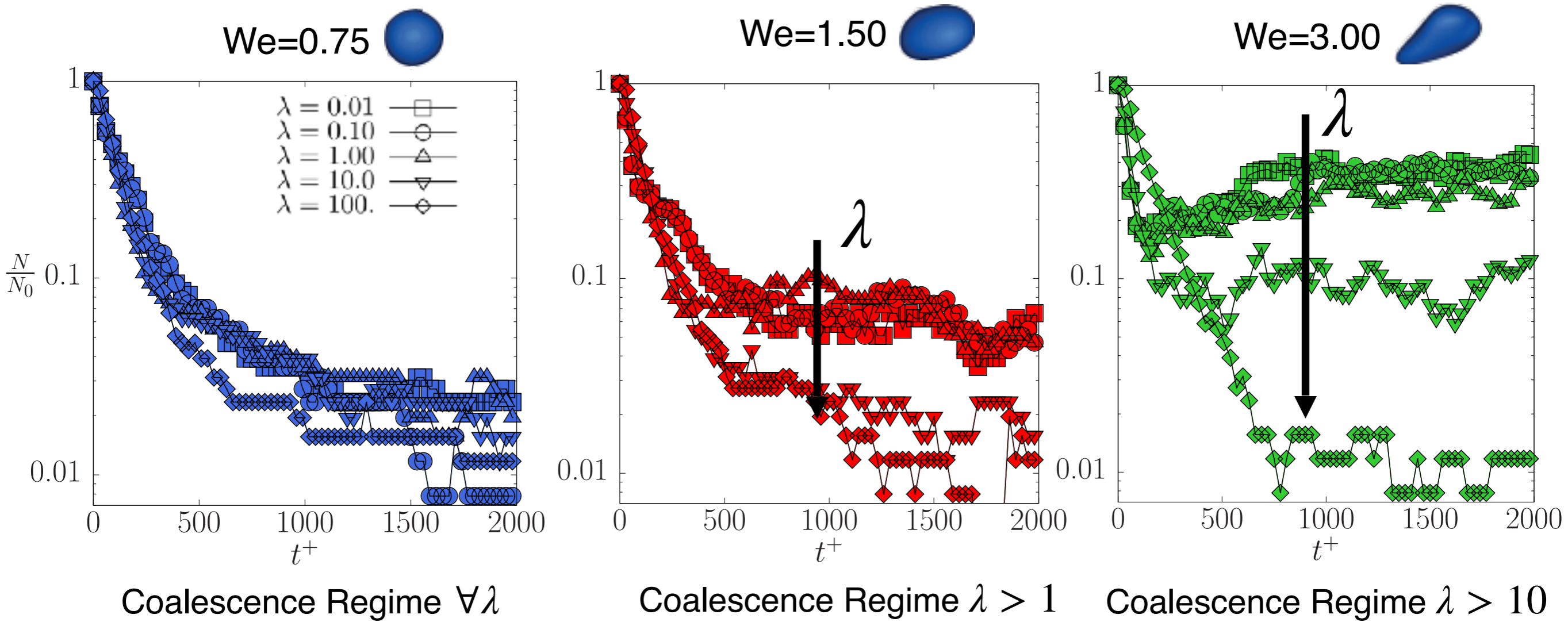
Low drops viscosity

λ

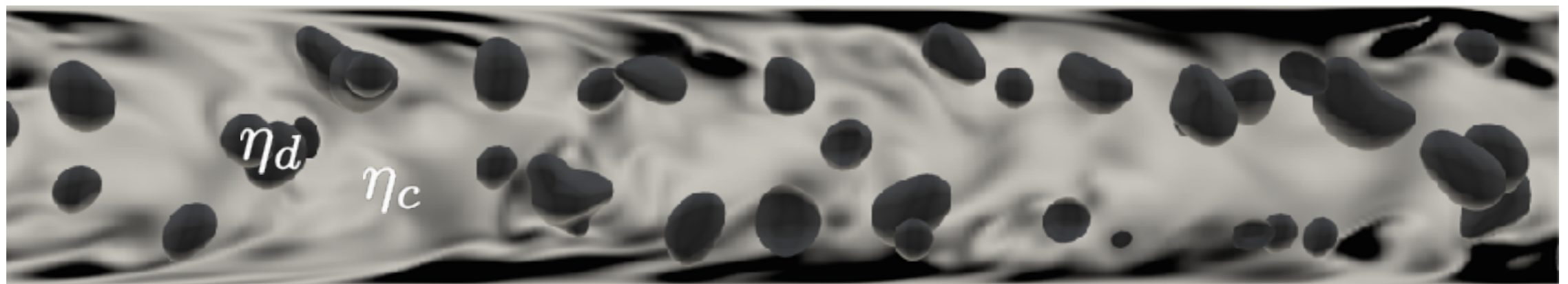
High drops viscosity

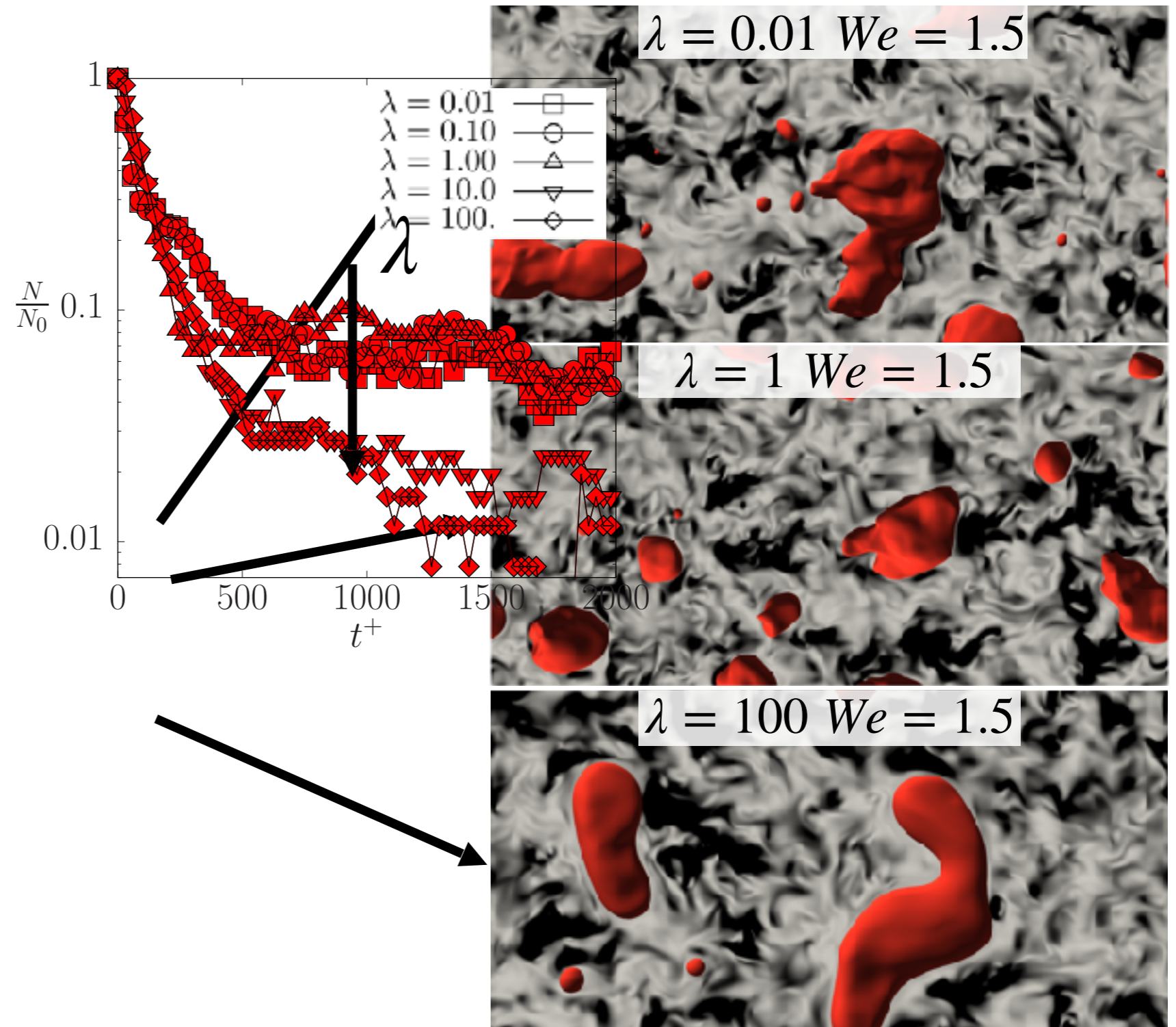
$$\lambda = \frac{\eta_d}{\eta_c}$$



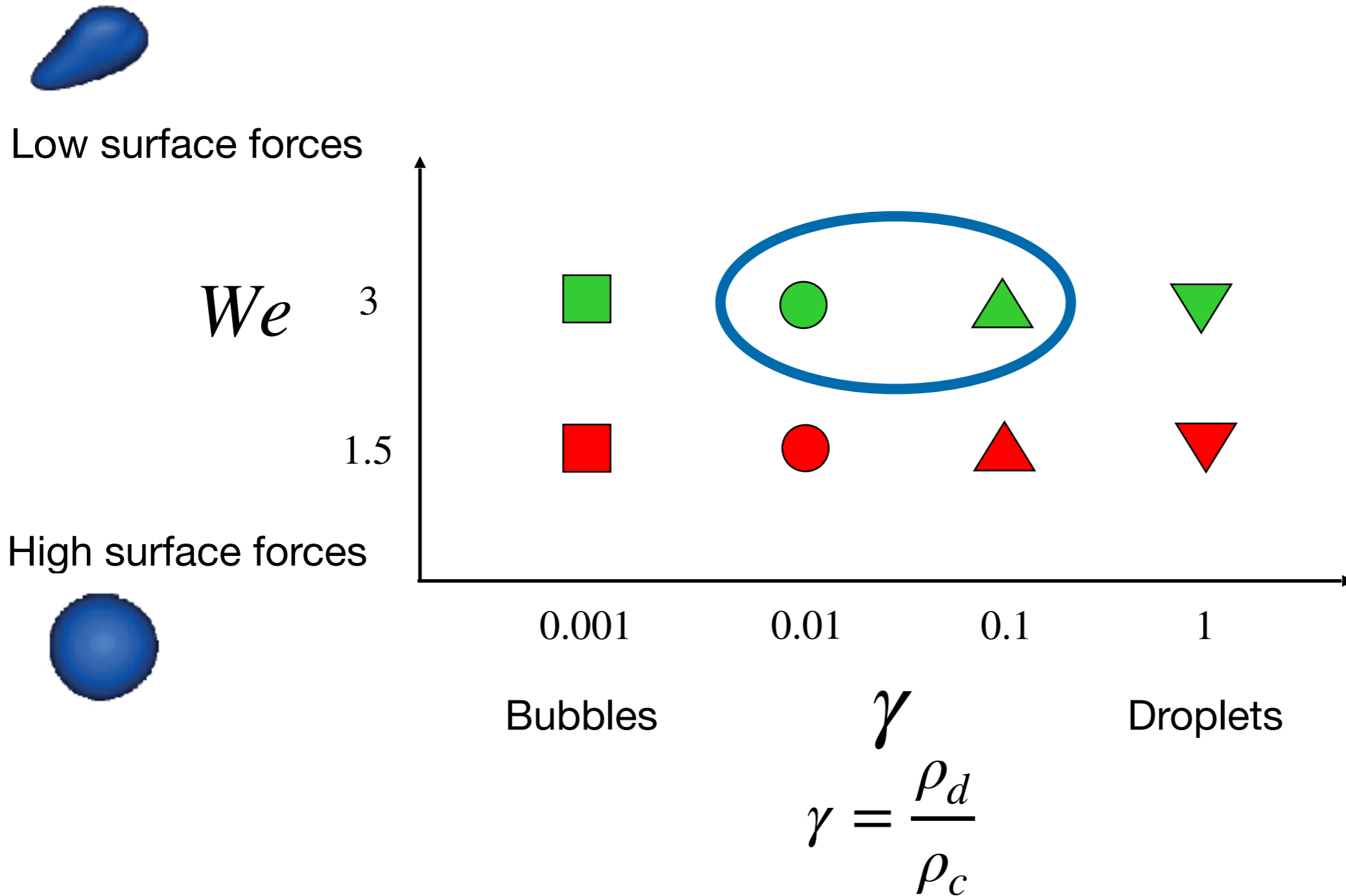


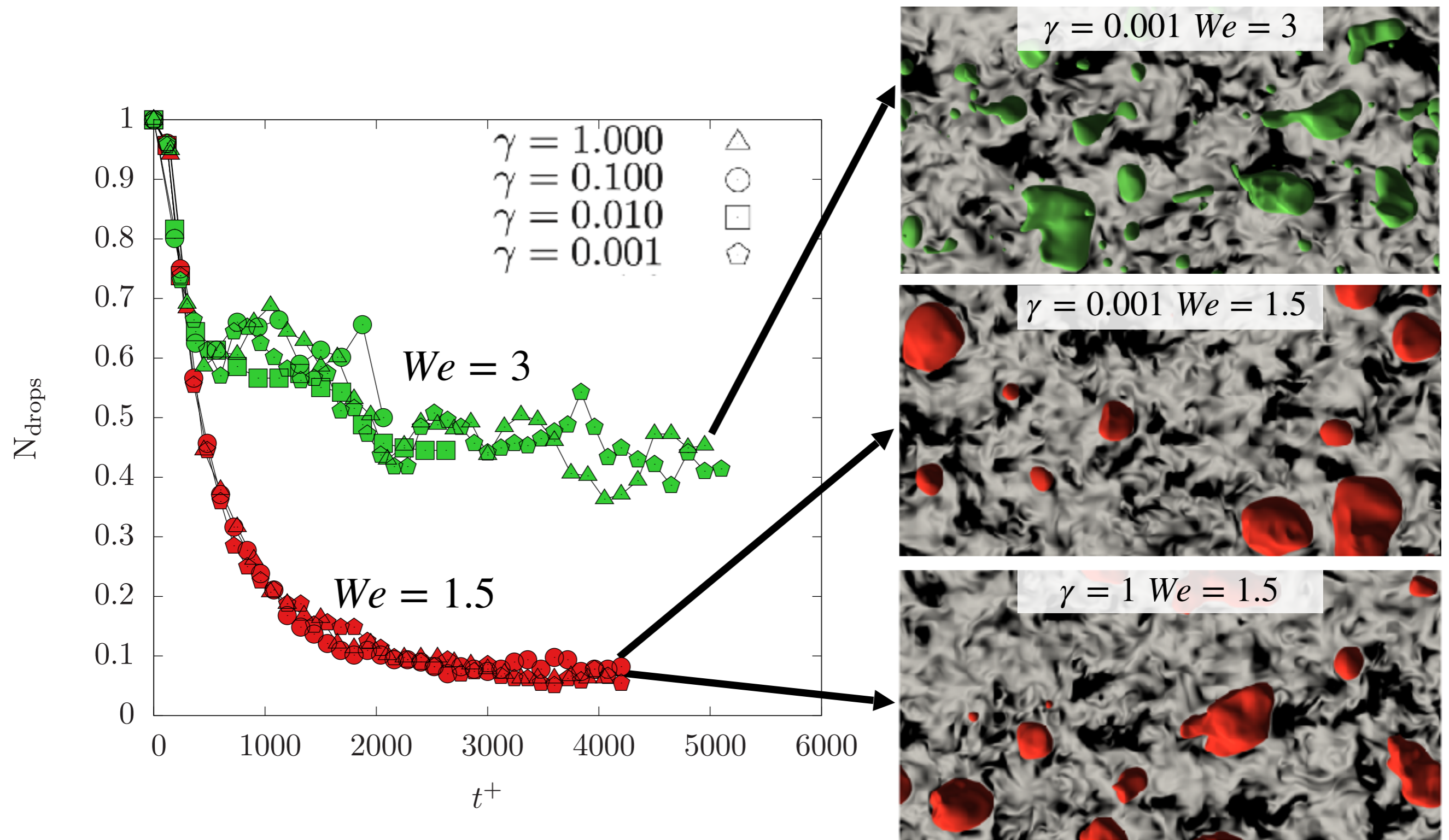
$$\lambda = \frac{\eta_d}{\eta_c}$$





Effect of density ratio and Weber number



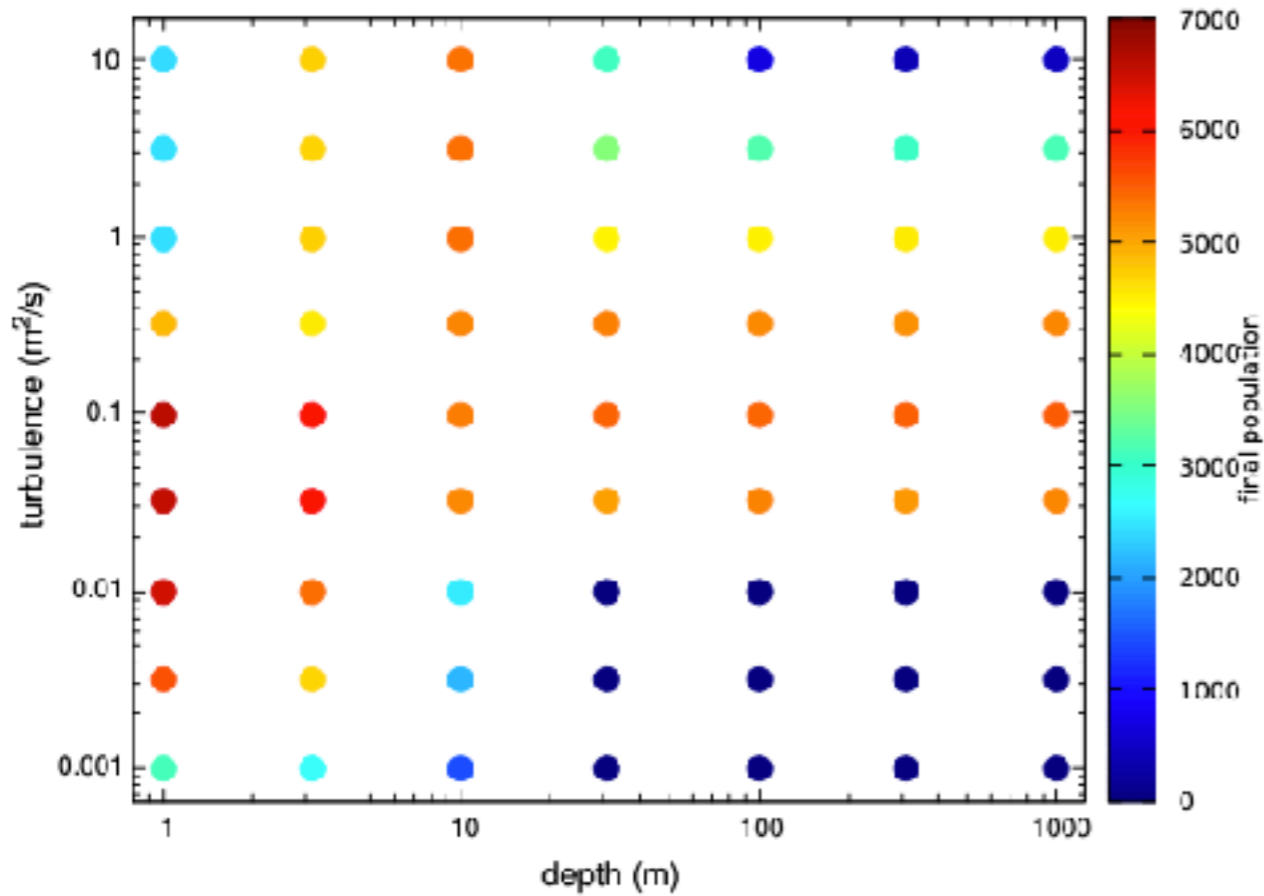


- Lowering Weber number increases resistance to breakage;
- Higher droplet viscosity leads to coalescence regime;
- Low density ratio does not seem to influence the number of droplets/bubbles.

Korteweg tensor:
Accounts for surface tension forces

$$\tau_c = |\nabla\phi|^2 \mathbf{I} - \nabla\phi \otimes \nabla\phi$$

Final population in D-z parameter space: reflective boundary



Deviation from Poisson distribution

